Costs

Project Global Coal Recovery

Site Name 37 and 62





AMD TREAT AMD TREAT MAIN COST FORM

| | | | · ·—· · · · · · · · · · |
|---------------------------|----------|----------|--|
| Passive Treatment | A | <u>s</u> | |
| Vertical Flow Pond | | | \$0 |
| Anoxic Limestone Drain | | | \$0 |
| Anaerobic Wetlands | | | \$0 |
| Aerobic Wetlands | | | \$0 |
| Manganese Removal Bed | 1 | 0 | \$116,772 |
| Oxic Limestone Channel | | | \$0 |
| Limestone Bed | | | \$0 |
| BIO Reactor | | | \$0 |
| Passive Subtotal: | | | \$116,772 |
| Active Treatment | | 3 | |
| Caustic Soda | | | \$0 |
| Hydrated Lime | 1 | 0 | \$111,398 |
| Pebble Quick Lime | | | \$0 |
| Ammonia | | | \$0 |
| Oxidants | | , | \$0 |
| Soda Ash | | | \$0 |
| Active Subtotal: | | | \$0 |
| Ancillary Cost | | | |
| Ponds | 1 | 0 | \$9,498 |
| Roads | | | \$0 |
| Land Access | | | \$0 |
| Ditching | 1 | 0 | \$4,195 |
| Engineering Cost | 1 | 0 | \$24,186 |
| Ancillary Subtotal: | - | | \$37,879 |
| Other Cost (Capital Cost) | | - | \$0 |
| Total Capital Cost: | | | \$266,049 |
| Annual Costs | | | |
| Sampling | 1 | 0 | \$1,736 |
| Labor | 1 | 0 | \$21,840 |
| Maintenance | 1 | 0 | \$7,324 |
| Pumping | | | \$0 |
| Chemical Cost | 1 | 0 | \$6,348 |
| Oxidant Chem Cost | 1 | | \$0 |
| Sludge Removal | 1 | 0 | \$3,637 |
| Other Cost (Annual Cost) |) | | \$0 |
| Land Access (Annual Cost) | | | \$0 |
| Total Annual Cost: | | | \$40,885 |
| Other Cost | T | <u> </u> | |
| 20101 0001 | <u> </u> | <u> </u> | VIIIIIIIIIIIIIIIIIIIIIIIIIIIIIIIIIIIII |

| | HWD LISEH I | |
|-------------------------------|-------------|-------|
| Water Quality | | |
| Calculated Acidity | 0.00 | mg/L |
| Alkalinity [| 0.00 | mg/L |
| Calculate Net Acidity (Acid-A | Alkalinity) | |
| Enter Net Acidity manually | | . 1 |
| Net Acidity (Hot Acidity) | 282.20 | mg/L |
| Design Flow | 200.00 | gpm |
| Typical Flow | 120.00 | gpm |
| Total Iron | 24.60 | mg/L |
| Aluminum | 22.10 | mg/L |
| Manganese | 10.00 | mg/L |
| рН | 3.40 | su |
| Ferric Iron | 0.00 | mg/L |
| Ferrous Iron | 0.00 | mg/L |
| Sulfate | 0.00 | mg/L |
| Filtered Fe | 0.00 | mg/L |
| Filtered Al | 0.00 | mg/L |
| Filtered Mn | 0.00 | mg/L |
| Specific Conductivity | 0.00 | uS/cm |
| Total Dissolved Solids | 0.00 | mg/L |
| Dissolved Oxygen | 0.00 | mg/L |
| | | |
| | | |

Total Annual Cost: per 1000 Gal of H2O Treated \$0.647 Company Name Project

Site Name

0.00

10.00

Manganese

mg/L

mg/L

22. Clear and Grub Unit Cost

AMD TREAT MANGANESE REMOVAL BED



Record Number 1 of 1

MN Removal Bed Name days Select One 1. Retention Time 1.00 **SIZING METHODS** 2. Limestone Needed tons 5.914.15 æ Based on Retention Time Tons of Limestone Needed Based on Tons of Limestone 3. Length at Top of Freeboard fť Tons of Limestone Needed 200.00 4. Width at Top of Freeboard ft Based on Dimensions Tons of Limestone Needed 919.45 hr/ft Based on Kinetics 5. Rate Constant (k) Tons of Limestone Needed 0.00 **Opening Screen** Manganese Removal Bed Sizing Summaries 1.00 inches 6. Stone Diameter Water Parameters 480.03 | ft 23. Top Length at Freeboard 5.00 mg/l 7. Effleunt Mn Concentration 244.01 | ft 23. Top Width at Freeboard Influent Water 35.00 8. % Void Space of Limestone Bed % **Parameters** 8,464 yd3 25. Freeboard Volume 107.53 lbs/ft3 9 Density of Loose Limestone that Affect ft2 111,410.7 26. Limestone Surface Area MN Removal Bed 12.00 10. Limestone Unit Cost \$/ton Calculated Acidity yd3 4,074.0 27. Limestone Volume 0.00 \$/yd3 11. Limestone Placement Unit Cost mg/L 0.00 tons 28. Tons of Limestone 5.914 2.00 12. Freeboard Depth Alkalinity 4.074 vd3 29. Excavation Volume 1.00 0.00 mg/L 13. Limestone Depth ft 30. Clear and Grub Area 4.0 acres 4.50 14. Excavation Unit Cost \$/yd3 Rise 31. Liner Area 14,935 | ft2 Calculate Net Acidity 2.0 : 1 15. Slope of Pond Sides 1.00 days 32. Theoretical Retention Time (Acid-Alkalinity) **Liner Cost Enter Net Acidity Manganese Removal Bed Sub-Totals** manually No Liner 70,970 \$ 33. Limestone Cost **Net Acidity** Clay Liner (Hot Acidity) 34. Limestone Placement Cost 0 \$ 16. Clay Liner Unit Cost \$/yd3 4.50 0.00 mg/L 18,333 ft 35. Excavation Cost 17. Thickness of Clay Liner 1.00 Synthetic Liner 36. Liner Cost 22,403 Design Flow 18. Synthetic Liner Unit Cost \$/yd2 200.00 gpm 37. Clear and Grub Cost 5,066 Typical Flow gpm ▼ 19. Clearing and Grubbing? 0.00 38. Total Cost 116,772 Total Iron 20. Land Multiplier 1.50 ratio 0.00 mg/L Aluminum C 21. Clear/Grub Acres acres

\$/acre

1256.00

Project Global Coal Recovery

Site Name 37 and 62

AMD TREAT HYDRATED LIME



| | | RMDT | REAT | |
|--------------------------------|---|--|---|-----------------|
| : | Hydrated Lime Name | | | |
| | 1. Annual Hydrated Lime 126,950.7 lbs/yr | 23. Mixing Tank (Assumes a Two Cell Mixing Tank) | 43. Polymer Feed System | \$ |
| Opening Screen Water Parameter | 2. Annual Hydrated Lime 63.4 tons/yr | | ✓ 44. Clearing and Grubbing? | |
| water Farameter | 3. Daily Hydrated Lime 347.8 Ibs/day | Cost Est based on Volume of Mixing Tank | | |
| Influent Water | 4. Pounds per Hour 14.492094 lbs/hr | 24. Tank Volume gal | 45. Clear and Grub Area | 2.00 acres |
| Parameters | 5. Purity of Hydrated Lime 96 % | Cost Est. based on Desired Retention Time | 46. Clear and Grub Costs | 1256.00 \$/acre |
| that Affect Hydrated Lime | 6 Mixing Efficency of 90 % | 25. Mixing Tank Volume 0.0 gal | Hydrated Lime Sizing | |
| Calculated Acidity | Hydrated Lime L | 26. Design Flow 200.00 gpm | 47. Tank Length | 0.0 ft |
| 0.00 mg/L | 7. Titration? Ibs of hydrated ime /aal | 27. Retention Time min | 48. Tank Width | 0.0 ft |
| 0.00 mg/L | 8. Titration Amount iime /gal of h2o | Specifications of Concrete Tank | 49. Tank Depth | 3 ft |
| | 9. Mechanical Aeration System 0.00 \$ | 28. Tank Wall Thickness ft | 50. Excavation Volume | 0.0 yd3 |
| Calculate Net Acidity | Silo Storage Quantity Price Refill Freq. Days | 29. Tank Bottom Thickness ft | for Mixing Tank 51. Volume of Concrete | |
| (Acid-Alkalinity) | 10. 20 Ton \$ 115 | 30. Tank Freeboardft | for Mixing Tank | 12 ft3 |
| | 11. ☐ 35 Ton \$ 201 | 31. Construction Labor Cost \$ | Hydrated Lime Cos | |
| manually Net Acidity | 12. 5 0 Ton \$ 287 | 32. Concrete Unit Cost \$/yd3 | 52. Silo(s) Cost | 0 \$ |
| (Hot Acidity) | 13. 6 0 Ton \$ 345 | 33. Excavation Unit Cost \$/yd3 | 53. Clarifier Cost | 98,886 \$ |
| 282.20 mg/L | 14. Clarifier | 34. Number of Motorized Mixers 2 qty | 54. Mixing Tank Cost | 0 \$ |
| Design Flow | C Cost of Clarifier \$ | 35. Unit Cost of Motorized Mixer 1000 \$ | 55. Construction Labor (Mixing Tank) | 0 \$ |
| Design Flow 200.00 gpm | C Cost Est based on Clarifier Diameter | 36. Number of Slide Gates 5 qty | 56. Excavation Cost (Mixing Tank) | 0 \$ |
| Typical Flow | 15. Diameter ft | 37. Unit Cost of Slide Gate 750 \$ | 57. Concrete Cost (MixingTank) | 0 \$ |
| 120.00 gpm | 16. Cost Muliplier Cost Est based on Flow | 38. Cost of Electric Panel 2000 \$ | 58. Motorized Mixer & Aeration Cost | 2,000 \$ |
| Total Iron 24.60 mg/L | 17. Design Flow 200.00 gpm | 39. Control Building | 59. Sweep and Blower Cost | 0 \$ |
| Aluminum | 18. Estimated Diameter 24.72 ft | | 60. Slide Gate Cost | 3,750 \$ |
| 22.10 mg/L | 19. Cost Muliplier 4000.0 | Cost of Control Building \$ | 61. Electric Control Panel Cost | 2,000 \$ |
| Manganese | | Cost Est. Based on Building Area | 62. Building Cost | 2,250 \$ |
| 10.00 mg/L | 20. Vibrator Air Sweep 0 | 40. Building Length 15 ft | 63. Polymer Feed System | 0 \$ |
| Record Number | 21. Pneumatic Air Sweep 0 | 41. Building Width 15 ft. | 64. Clear and Grub Cost | 2,512 \$ |
| 1 of 1 | 22. Blower Blocks 0 | 42. Building Unit Cost 10.0 \$/ft2 | 65. Total Cost | 111,398 |
| <i></i> | | L | ' | |

Company Name Project

Site Name

AMD TREAT PONDS



| Pond Name | | | | |
|-----------|---------------------|--|-------------------------------------|--------------------|
| | | Pond Design Based On: | 23. Revegetation Cos | st 1500.00 \$/acre |
| | | Retention Time | 24. Number of Ponds for this Design | n 1 number |
| | | 1. Desired Retention Time 24.0 hours | 25. Cost of Baffle | s 0 \$ |
| | | 3. Sludge Removal Frequency 1.00 times/year | Calculated Pond Dimensi | ons per Pond |
| | ing Screen | 4. Titration? | 26. Length at Top of Freeboard | 161 ft |
| water | Parameters | gal sludge/ | 27. Width at Top of Freeboard | 84 ft |
| Influe | nt Water | 5. Sludge Rate gal H2O | 28. Freeboard Volume | 2,427 yd3 |
| | ameters : Affect | O. T Groom Solids | 29. Water Volume | 1,485 yd3 |
| | onds | 7.Sludge Density 8.35 lbs./gal | 30. Estimated Annual Sludge | 59 yd3/yr |
| | ated Acidity | C Pond Size | 31. Volume of Sludge | 59 yd3/ remova |
| ļ —— | 0.00 mg/L | 8. Pond Length at Top of Freeboard ft | per Removal | 0.92 acre ft |
| | linity 0.00 mg/L | 9. Pond Width at Top of Freeboard ft | 33. Excavation Volume | 1,485 yd3 |
| | | Run Rise | 34. Clear and Grub Area | 0.47 acres |
| Calculate | late Net | 10. Slope Ratio of Pond Sides 2.0 : 1 | 35. Liner Area | 888 yd2 |
| Acidity | y Alkalinity) | 11. Freeboard Depth 2.0 ft | 36. Calculated Retention Time | 24 hours |
| l i | Net Acidity | 12. Water Depth 4.0 ft | Ponds Sub-1 | otals per Pond |
| | ually | | 37. Excavation Cost | 7,676 \$ |
| | Acidity | 13. Excavation Unit Cost 4.50 \$/yd3 14. Total Length of Effluent 6.00 ft | 38. Pipe Cost | 0 \$ |
| 11 | Acidity) | / Influent Pipe 0.00 ft | 39. Liner Cost | 993 \$ |
| | 0.00 mg/L | 15. Unit Cost of Pipe 0.00 \$/ft | 40. Clearing and Grubbing Cost | 591 \$ |
| Design | Flow | Liner Cost | 41. Revegetation Cost | 235 \$ |
| 1 1 | 00.00 gpm | Clay Liner | 42. Baffle Cost | 0 \$ |
| Typica | | 16. Clay Liner Unit Cost 4.50 \$/yd3 | | |
| Total Ir | | 17. Thickness of Clay Liner 1.0 ft | 43. Estimated Cost | 9,498 \$ |
| <u> </u> | 24.60 mg/L | C Synthetic Liner | | |
| Alumin | | 18. Synthetic Liner Unit Cost \$/yd2 | | |
| Manga | 22.10 mg/L nnese | ✓ 19. Clearing and Grubbing? | | |
| | 10.00 mg/L | | | |
| Poo | ord Number | C 21. Clear/Grub Acres | S | |
| 1 0 | | 22. Clear and Grub Unit Cost 1256.00 \$/acc | re | |

Project Global Coal Recovery

Site Name 37 and 62

AMD TREAT DITCHING



| Ditching Name | | | |
|---|--------------------------------|---------|---------|
| 1. Ditch Length Rock 100 ft | 13. Ditch Depth of Rock | 1.50 | ft |
| 2. Ditch Length Grass 100 ft | 14. Cost of Ditch Surface Rock | 18.00 | \$/yd3 |
| 3. Bottom Width of Ditch 4.0 ft | 15. Cost to Place Rock | 12.00 | \$/yd3 |
| 4. Ditch Depth 3.00 ft | 16. Excavation Unit Cost | 4.50 | \$/yd3 |
| 5. Geo Textile Unit Cost 0.50 \$/yd2 | 17. Length of Silt Fence | 0.00 | ft |
| 6. Length of Geo Textile 100 ft | 18. Unit Cost of Silt Fence | 1.00 | \$/ft |
| 7 Slana Ratio of Run Rise | 19. Revegetation Unit Cost | 1500.00 | \$/acre |
| 7. Slope Ratio of Ditch Sides 2.00 1.00 | Ditching Sub | -Totals | |
| ■ 8. Surveying? | 20. Excavation Cost | 1,000 | \$ |
| 9. Survey Rate acres/day | 21. Survey Cost | 0 | \$ |
| 10. Survey Unit Cost \$/day | 22. Clear and Grub Cost | 111 | \$ |
| ☐ 11. Clearing and Grubbing? | 23. Aggregate Cost | 2,903 |] \$ |
| 12. Clear and Grub Cost 1256.00 \$/acre | 24. Filter Fabric Cost | 97 | \$ |
| | 25. Silt Fence Cost | 0 | \$ |
| | 26. Revegetation Cost | 84 | \$ |
| Record Number 1 of 1 | 27. Total Cost | 4,195 |] \$ |

Project Global Coal Recovery

Site Name 37 and 62

AMD TREAT ENGINEERING COST

1. Capital Cost * 241,864 2. Per Cent of Capital Cost % 10.00 \$ 4. Total Engineering Cost 24,186 \$

> * Total Capital Cost minus Engineering and Land Access Capital Cost

Printed on 08/21/2007



Sampling Name

Project Global Coal Recovery

Site Name 37 and 62

AMD TREAT

SAMPLING



| ← Estimate Sampling Cost | |
|--------------------------------|-------------------|
| 1. Unit Labor Cost | 35.00 \$/hr |
| 2. Collection Time per Sample | 0.33 hours/sample |
| 3. Travel Time | 1.00 hr |
| 4. Sample Frequency | 1.00 samples/mo |
| 5. Lab Cost Per Sample | 25.00 \$/sample |
| 6. Number of Sample Points | 3 points |
| C Enter Established Annual Sa | mpling Cost |
| 7. Actual Annual Sampling Cost | \$ |

Sampling Sub-Totals

8. Yearly Sample Analysis Cost

900 \$

9. Yearly Travel Cost

420 \$

10. Yearly Collection Cost

416 \$

11. Sampling Cost

1,736 \$

Record Number 1 of 1

Project Global Coal Recovery

Site Name 37 and 62

AMD TREAT

LABOR



| (| Estimate Labor Cost | |
|----------|----------------------------------|---------------|
| | 1. Site Visits per Week | 3.00 |
| | 2. Site Labor Time per Visit | 2.00 hours |
| | 3. Travel Time per Visit | 2.00 hours |
| | 4. Unit Labor Cost | 35.00 \$/hour |
| ~ E | Enter Established Annual Labor (| Cost |
| | 5. Actual Annual Labor Cost | \$ |

Record Number 1 of 1

Project

Global Coal Recovery

Site Name

37 and 62

AMD TREAT

MAINTANENCE

1. Percent of Active Cost 3.00 %

2. Percent of Passive Cost 3.00 %

3. Percent of Ancillary Cost * 3.50 %

4. Percent of Other Capital Cost 3.50 %

C Enter Established Annual Maintenance Cost

5. Annual Maintenance Cost

Maintenance Sub-Totals

6 Total Maintenance Active Cost 3,342 \$

Cost 3,503 \$

7. Total Maintenance Passive Cost8. Total Maintenance Ancillary Cost

479 \$

9. Total Maintenance Other Capital Cost

0 \$

10. Total Maintenance Cost

7,324 \$



^{*} Ancillary Cost does int include Cost for Land Access and Engineering Cost

Project Global Coal Recovery

Site Name 37 and 62

AMD TREAT CHEMICAL COST



Chemical Cost Name: E. Anhydrous Ammonia ? A. Hydrated Lime ? **Opening Screen** 21. Titration? Water Parameters 1 Titration? lbs of ammonia lbs of hydrated 22. AmmoniaTitration Amount 2. Hydrated Lime Titration Amount / gal H2O lime / gal of H2O Influent Water % 23. Ammonia Purity 3. Hydrated Lime Purity 96.00 | % **Parameters** % 24. Mixing Efficiency of Ammonia that Affect 4. Mixing Efficiency of Hydrated Lime 90.00 **Chemical Cost** Non-Bulk Delivery 5. Hydrated Lime Unit Cost 0.0500 \$/lb Calculated Acidity \$/lb 25. Ammonia Non-Bulk Unit Cost 0.00 | mg/L C B. Pebble Quick Lime? Bulk Delivery Alkalinity 6. Titration? 26. Ammonia Bulk Unit Cost \$/lb 0.00 mg/L lbs of Pebble 7. Pebble Lime Titration Amount Lime / gal of H2O F. Soda Ash? 8. Pebble Lime Purity % Calculate Net 27. Titration? Acidity % 9. Mixing Efficiency of Pebble Lime ibs of soda ash 28 Soda Ash Titration Amount (Acid-Alkalinity) / gal of H2O O Delivered in Bags Enter Net Acidity 29. Soda Ash Purity % manually \$/lb 10. Pebble Lime Bag Unit Cost 30. Mixing Efficiency of Soda Ash % Net Acidity Bulk Delivery (Hot Acidity) \$/lb 11. Pebble Lime Bulk Unit Cost 31 Soda Ash Unit Cost \$/lb 282.20 mg/L C. Caustic Soda? G. Known Chemical Cost? 12. Titration? 32. Known Annual Chemical Cost S Design Flow gal ofcaustic **Annual Amount of** 13. Caustic Titration Amount 200.00 gpm / gal H2O **Chemical Cost Sub-Totals** Chemicals Consumed purity of 20% Typical Flow 14. Caustic Purity 33. Total Hydrated Lime Cost 6,348 126,950 caustic solution 120.00 gpm 15. Mixing Efficiency of Caustic 34. Total Pebble Lime Cost 0 Total Iron Non-Bulk Delivery S 35. Total Caustic Soda Cost gals 24.60 mg/L \$/gal 16. Caustic Non-Bulk Unit Cost Aluminum \$ 36. Total Limestone Cost tons 0 0 Bulk Delivery 22.10 mg/L 37. Total Anhydrous Ammonia Cost \$ lbs 0 0 \$/gal 17. Caustic Bulk Unit Cost Manganese \$ 38. Total Soda Ash Cost lbs 0 10.00 | mg/L C D. Limestone? \$ 39. Total Known Chemical Cost 18. Limestone Purity % **Record Number** 40. Selected Chemical: HYDRATED LIME % 19. Limestone Efficiency Annual Chemical Cost \$ 6.348 20 Limestone Unit Cost 1.of 1 \$/ton

Project Global Coal Recovery

Site Name 37 and 62

AMD TREAT SLUDGE REMOVAL



| Opening Screen | | SLODGE RE | LIVIOVAL | THAID I IZEMI |
|---------------------------------------|----------------------------|------------------------------------|-----------|--|
| Water Parameters | Sludge Removal Name | | | |
| Influent Water Parameters that Affect | 1. Select One | Selection for Me of Removing SI | | 14. Iron Concentration 24.60 mg/L |
| Sludge Removal | Sludge Removal by | / \$ per Gallon | | 15. Manganese Concentration 10.00 mg/L |
| Calculated Acidity 0.00 mg/L | 2. Sludge Removal U | Jnit Cost 0.0 |)5 \$/gal | 16. Aluminum Concentration 22.10 mg/L |
| Alkalinity | | / Vacuum Truck | | 17. Total Miscellaneous Concentration 0 mg/L |
| 0.00 mg/L | 3. Vacuum Truck l | Jnit Cost | \$/hr | 18. Percent Solids 5.00 % |
| | 4. Mobilizat | ion Cost | \$ | 19. Sludge Density 8.33 lbs/gal |
| Calculate Net Acidity | 5. Hours to | <u> </u> | hr | ☐ 20 Titration? |
| (Acid-Alkalinity) | C Sludge Removal by | | ion | 21. Gal. of Sludge per Gal of Water Treated gal |
| Enter Net Acidity manually | 6. Mechanical Excavation U | Init Rate | \$/hr | 21. Gai. Of Sludge per Gar of Water Treated |
| Net Acidity | 7. Mobilizat | ion Cost |] \$ | 22. Estimated Sludge Volume 360 yd3/yr |
| (Hot Acidity) | 8. Hours to | be Used | hr | |
| 282.20 mg/L | C Sludge Removal by | / Lagoon Cleaner | | Cost for Sludge Removal Types |
| Design Flow | 9. Lagoon Cleaning L | Init Rate | \$/hr | 23. Removal by \$ per Gallon 3,637 |
| 200.00 gpm | 10. Mobilizat | | - s | 24. Removal by Vacuum Truck 0 |
| Typical Flow | | | 글 ` | 25. Removal by Mechanical Excavation 0 \$ |
| 120.00 gpm | 11. Hours to | be Used | 」 hr | 26. Removal by Lagoon Cleaner 0 \$ |
| Total Iron 25 mg/L | C Actual Sludge Rem | oval Cost | | 27. Actual Sludge Removal Cost 0 \$ |
| Aluminum | 12. Actual Sludge Remo | val Cost | \$ | Sludge Removal Sub-Totals |
| 22 mg/L | | | | Clauge Removal cab-loads |
| Manganese 10 mg/L | 13. Off Site Dispo | sal Cost 0.0 | 0 \$ | 28. Currently Selected Removal Cost Plus Off Site Disposal Cost 3,637 \$ |
| : | Record Number | 1 of 1 | ` | |

Project

Global Coal Recovery

Site Name 37 and 62

AMD TREAT RECAPITIZALITION COST



Calculation Period 75 yrs Inflation Rate 3.10 % Net Return Rate 6.00 %

| Α. | В | С | D | E | F | G |
|---------------------|-----------------------|----------|--------------------|---------------|----------------------|---------------------------------------|
| Description of Item | Unit Cost Per Item | Quantity | Total Item Cost | Life Cycle | Number of Periods | Total PV |
| 1. Mn Removal Bed | 116,772 | 1 | 116,772 | 15 | 5 | 198,032 |
| 2. Pond | 9,498 | 1 | 9,498 | 15 | 5 | 16,108 |
| 3. | 0 | 0 | 0 | 0 | 0 | 0 |
| 4. | 0 | 0 | 0 | 0 | 0 | 0 |
| 5. | 0 | 0 | 0 | 0 | 0 | C |
| 6. | 0 | 0 | 0 | 0 | 0 | (|
| 7. | 0 | 0 | 0 | 0 | 0 | |
| 8. | 0 | 0 | 0 | 0 | 0 | |
| 9. | 0 | 0 | 0 | 0 | 0 | |
| 0. | 0 | 0 | 0 | 0 | 0 | |
| 1. | 0 | 0 | 0 | 0 | 0 | · · |
| 2. | 0 | 0 | 0 | 0 | 0 | |
| 3. | 0 | 0 | 0 | 0 | 0 | |
| 4. | 0 | 0 | 0 | 0 | 0 | · · · · · · · · · · · · · · · · · · · |
| 5. | 0 | 0 | 0 | 0 | 0 | |
| 16. | 0 | 0 | 0 | 0 | 0 | (|
| 7. | 0 | 0 | 0 | 0 | 0 | (|
| 18. | 0 | 0 | 0 | 0 | 0 | (|
| 19. | 0 | 0 | 0 | 0 | 0 | (|
| 20. | 0 | 0 | 0 | 0 | 0 | |

Total Capital Cost

126,270 \$ PV Grand Total

214,140