

MarkWest Liberty Midstream & Resources, L.L.C. 1515 Arapahoe Street Tower 1, Suite 1600 Denver, CO 80202-2126 (800) 730-8388 (303) 290-8700 (303) 825-0920 Fax

June 28, 2022

Mr. Mark Gorog Regional Air Quality Manager PA DEP SW Regional Office 400 Waterfront Drive Pittsburgh, PA 15222



Re: MarkWest Liberty Midstream & Resources, L.L.C. Harmon Creek Gas Plant Plan Approval Application

Dear Mr. Gorog:

MarkWest Liberty Midstream & Resources, L.L.C. (MPLX) hereby submits a plan approval application for the Harmon Creek Gas Plant located at 123 Point Pleasant Rd in Smith Township, Washington County. The Harmon Creek Gas Plant is currently authorized to operate under GP1-63-01011A and GP5-63-01011A. MPLX seeks authorization to install and operate equipment associated with Harmon Creek Cryo II. In addition to the equipment currently authorized at the facility, MPLX proposes the installation and operation of the following equipment at the facility:

- One (1) 260 mmscfd natural gas processing plant;
- One (1) Cryo plant regenerative heater rated at a maximum heat input of 19.62 MMBtu/hr;
- One (1) 500-gallon methanol storage tank;
- Three (3) electric-driven compressors and associated rod-packing venting; and
- Associated fugitive components.

De minimis emission increases associated with the existing pigging and truck loadout operations, in addition to emissions from maintenance blowdowns and some PSVs will be controlled by the existing process flare.

The following are included with this submittal:

- General Information Form
- Compliance Review Form
- Plan Approval Application Forms
- Proof of Municipal Notification
- Process Flow Diagram
- Detailed Emission Estimates
- Manufacturer's Information

If you have any questions about this application, please contact me at (412) 815-8886 or via email at <u>ajuarez@marathonpetroleum.com</u>.

Sincerely,

Alexandra M. Juary

Alexandra M. Juarez G&P Engineer I

General Information Form

COMMONWEALTH OF PENNSYLVANIA DEPARTMENT OF ENVIRONMENTAL PROTECTION

GENERAL INFORMATION FORM – AUTHORIZATION APPLICATION

Before completing this General Information Form (GIF), read the step-by-step instructions provided in this application package. This form is used by the Department of Environmental Protection (DEP) to inform our programs regarding what other DEP permits or authorizations may be needed for the proposed project or activity. This version of the General Information Form (GIF) must be completed and returned with any program-specific application being submitted to the DEP.

Related ID#s ((If Known)		DEP	USE ON	LY	
Client ID#	APS ID#	Da	te Recei	ved & Gene	ral Notes	
Site ID# 823541	Auth ID#					
Facility ID# 819388						
	CLIENT INFORMA	TION				
DEP Client ID#	Client Type / Code OWOP	Dun &	Brade	street ID#		
Legal Organization Name or Regist	tered Fictitious Name	Employer ID# (EIN)	Is the El	N a SSI	٧?
MarkWest Liberty Midstream and Res	sources, L.L.C.	30-0528059		🗌 Yes	\boxtimes	NO
State of Incorporation or Registration	ion of Fictious Name 🛛 🗆 Co	rporation 🛛 LL(Partnershi	p 🗌 LI	LP 🗌 LP
Delaware	🗌 So	e Proprietorship		Associatio	n/Organ	ization
		ate/Trust 🗌 Oth	ner			
Individual Last Name	First Name	МІ	Suffi	x		
Additional Individual Last Name	First Namo	MI	Suff:	v		
Additional mulvidual East Name	First Name		Sum	•		
Mailing Address Line 1	Mailin	g Address Line 2	2			
1515 Arapahoe St.	Tower	1, Suite 1600				
Address Last Line – City	State	ZIP+4	C	ountry		
Denver	CO	80202-2137	U	SA		
Client Contact Last Name	First Name	M	I	S	uffix	
Juarez	Allie	M				
Client Contact Title	Phon	e E	xt	C	ell Pho	ne
	412-8	15-8886				
Email Address				70 4054		
ajuarez@marathonpetroleum.com			303-5	/ 3-4954		
	SITE INFORMAT	ION				
DEP Site ID# Site Name						
823541 Harmon Creek G	Bas Plant					
EPA ID#	Estimated Number of Emplo	yees to be Pres	ent at	Site	25	
Description of Site						
Natural Gas Processing Plant						
County Nome(c) Mu	aininglity/inc)		City	Poro	Twn	Stata
<u>Vashington</u>	th					
	ui		+			ГA
			\exists			
			\exists			
Site Location Line 1	Site Lo	cation Line 2				
123 Point Pleasant Rd	0.10 20					
Site Location Last Line – City	State	ZIP+4				
Bulger	PA	15019				
Detailed Written Directions to Site						

From Pittsburgh head west on Hwy 22 to Exit 60A, stay left on Steubenville Pike (0.9 mi.), turn left onto Creek Road (0.5 mi.), keep left to stay on Point Pleasant Road (1.3 mi.), turn left into Harmon Creek Gas Plant

Site Contact Last Name		First Name		Γ	MI	Suffix
Ettore		David		(G	
Site Contact Title			Site Conta	ct Firm		
Environmental Supervisor			MarkWest I	_iberty Midstrea	am and Resour	ces, L.L.C.
Mailing Address Line 1			Mailing Ad	dress Line 2		
4600 J. Barry Court			Suite 500			
Mailing Address Last Lin	e – City		State	ZIP+4		
Canonsburg	-		PA	15317		
Phone	Ext	FAX	Email Add	ress		
724-873-2803			DGEttore@	marathonpetro	leum.com	
NAICS Codes (Two- & Three	e-Digit Codes	s – List All That Apply)		6-Digit	Code (Optiona	l)
211130				NA		
Client to Site Relationshi	р					
OWNOP						

FACILITY INFORMATION

No

 \boxtimes

Yes

Modification of Existing Facility

Will this project modify an existing facility, system, or activity? 1. 2.

Will this project involve an addition to an existing facility, system, or activity? If "Yes", check all relevant facility types and provide DEP facility identification numbers below.

	Facility Type	DEP Fac ID#	Facility Type	DEP Fac ID#
\boxtimes	Air Emission Plant	819388	Industrial Minerals Mining Operation	
	Beneficial Use (water)		Laboratory Location	
	Blasting Operation		Land Recycling Cleanup Location	
	Captive Hazardous Waste Operation		Mine Drainage Treatment / Land Recycling Project Location	
	Coal Ash Beneficial Use Operation		Municipal Waste Operation	
	Coal Mining Operation		Oil & Gas Encroachment Location	
	Coal Pillar Location		Oil & Gas Location	
	Commercial Hazardous Waste Operation		Oil & Gas Water Poll Control Facility	
	Dam Location		Public Water Supply System	
	Deep Mine Safety Operation -Anthracite		Radiation Facility	
	Deep Mine Safety Operation -Bituminous		Residual Waste Operation	
	Deep Mine Safety Operation -Ind Minerals		Storage Tank Location	
	Encroachment Location (water, wetland)		Water Pollution Control Facility	
	Erosion & Sediment Control Facility		Water Resource	
	Explosive Storage Location		Other:	

Latitude/Longitude	Latitude			Longitude		
Point of Origin	Degrees	Minutes	Seconds	Degrees	Minutes	Seconds
Harmon Creek Gas Plant	40	24	4	80	21	26
Horizontal Accuracy Measure	Feet		or-	- Me	eters	
Horizontal Reference Datum Code	□ Nor □ Nor ⊠ Wo	th American th American rld Geodetic \$	Datum of 192 Datum of 198 System of 19	27 33 184		
Horizontal Collection Method Code						
Reference Point Code						
Altitude	Feet 1	171	or-	- Me	eters	
Altitude Datum Name	🗌 The	National Ge	odetic Vertic	al Datum of '	1929	
	🗌 The	North Ameri	can Vertical	Datum of 198	88 (NAVD88)	
Altitude (Vertical) Location Datum Colle	ection Meth	od Code				
Geometric Type Code						
Data Collection Date						
Source Map Scale Number		Inch(es)	=		Feet	
Or		Centimete	r(s) =		Meter	S

PROJECT INFORMATION

Project Name										
Harmon Creek Gas Plant GP-5 Modification										
Proposed cons	truction :	and operati	on of Harmon Cree	k 2 which in	-ludes t	hroo ('	R) electr	ic-driven c	omores	sors and
associated blov	vdowns/v	venting on	e (1) 19 62 MMBtu	/hr regenerati	on heat	er and		iated funitiv	/e comr	onents
Project Consu	Itant La	st Name	First N	Name	onnoat	or, and	<u>MI</u>	latoa lagiti	Suffix	
None used		otituiito							C ullix	
Project Consu	Itant Tit	le		Consultin	g Firm					
Mailing Addres	ss Line	1		Mailing A	ddress	Line 2	2			
Address Last	Line – C	ity		State			ZIP+4			
Dhama		F 4	FAV							
Phone		EXt	FAX	Email A	aaress					
Time Schedule	es	Project M	lilestone (Optiona	al)						
								N		
1. Is the pr	oject loo	cated in or	within a 0.5-mile	radius		Yes	\boxtimes	NO		
of an	Environ	imental J	ustice communit	ty as						
denned		ſ								
To d	letermine	if the projec	t is located in or with	in a 0.5-mile ra	dius of a	an envi	ronment	al justice co	mmunity	, please use
the o	online <u>Env</u>	/ironmental	Justice Areas Viewer							
2. Have yo	ou infori	med the s	urrounding com	nunity	\boxtimes	Yes		No		
prior to	o subn	nitting the	e application to	b the						
Departm	nent?	-								
		_								
Method	of notifi	cation: Mu	nicipal notifications p	er 25 Pa. Cod	<u>e</u>					
<u>§ 127.41</u>	3		•4	- 41 - 4		Vaa		Ne		N1/A
3. Have yo	ou addr	essea cor	nmunity concerns	s that		res		INO		IN/A
lf no	ntineu r	oriefly descri	be the community co	ocerns that hav	ve been i	express	sed and	not address	ed	
1110	, piedee c				0.00011	onproo				
4. Is your p	oroject f	unded by s	state or federal grades	ants?		Yes	\boxtimes	No		
Note: If	f "Yes", sp	ecify what a	spect of the project is	s related to the	grant ar	nd prov	ide the g	rant source,	contact	person
a	and grant	expiration da	ate.							
Δ	spect of F	Project Relat	ed to Grant							
Grant Contact Person:										
			an authoritati			Vac		No		
5. Is this	applica	ation for	an authorizatio	n on		res	凶	NO		
reference	IX A 01	see Annor	iu use Policy? ndix A of the Lan	(ror d lise						
Policy a	ttached	to GIF iner	ructions)	u U3 c						
Note: If	"No" to C	Question 5. th	ne application is not s	ubject to the L	and Use	Policy.				
lf	"Yes" to	Question 5.	the application is sub	ject to this poli	cy and th	ne Appl	icant sho	ould answer	the addi	tional
n	questions in the Land Use Information section.									

LAND USE INFORMATION

<u>Note</u>: Applicants should submit copies of local land use approvals or other evidence of compliance with local comprehensive plans and zoning ordinances.

1.	Is there an adopted county or multi-county comprehensive plan?		Yes		No
2.	Is there a county stormwater management plan?		Yes		No
3.	Is there an adopted municipal or multi-municipal comprehensive		Yes		No
	plan?				
4.	Is there an adopted county-wide zoning ordinance, municipal zoning		Yes		No
	ordinance or joint municipal zoning ordinance?				
	Note: If the Applicant answers "No" to either Questions 1, 2 or 3, the provisions	of the PA N	IPC are no	ot appli	cable and the
	Applicant does not need to respond to questions 4 and 5 below.				
	If the Applicant answers "Yes" to questions 1, 2 and 3, the Applicant shou	Id respond	to questior	ns 4 ar	nd 5 below.
5.	Does the proposed project meet the provisions of the zoning		Yes		No
	ordinance or does the proposed project have zoning approval? If				
	zoning approval has been received, attach documentation.				
6.	Have you attached Municipal and County Land Use Letters for the		Yes		No
	project?				

COORDINATION INFORMATION

<u>Note</u>: The PA Historical and Museum Commission must be notified of proposed projects in accordance with DEP Technical Guidance Document 012-0700-001 utilizing the Project Review Form.

If the activity will be a mining project (i.e., mining of coal or industrial minerals, coal refuse disposal and/or the operation of a coal or industrial minerals preparation/processing facility), respond to questions 1.0 through 2.5 below.

If the activity will not be a mining project, skip questions 1.0 through 2.5 and begin with question 3.0.

1.0	Is this a coal mining project? If "Yes", respond to 1.1-1.6. If "No", skip to Question 2.0	Yes	\boxtimes	No
1.1	Will this coal mining project involve coal preparation/ processing activities in which the total amount of coal prepared/processed will be equal to or greater than 200 tons/day?	Yes		No
1.2	Will this coal mining project involve coal preparation/ processing activities in which the total amount of coal prepared/processed will be greater than 50,000 tons/year?	Yes		No
1.3	Will this coal mining project involve coal preparation/ processing activities in which thermal coal dryers or pneumatic coal cleaners will be used?	Yes		No
1.4	For this coal mining project, will sewage treatment facilities be constructed and treated waste water discharged to surface waters?	Yes		No
1.5	Will this coal mining project involve the construction of a permanent impoundment meeting one or more of the following criteria: (1) a contributory drainage area exceeding 100 acres; (2) a depth of water measured by the upstream toe of the dam at maximum storage elevation exceeding 15 feet; (3) an impounding capacity at maximum storage elevation exceeding 50 acre-feet?	Yes		No
1.6	Will this coal mining project involve underground coal mining to be conducted within 500 feet of an oil or gas well?	Yes		No
2.0	Is this a non-coal (industrial minerals) mining project? If "Yes", respond to 2.1-2.6. If "No", skip to Question 3.0.	Yes	\boxtimes	No
2.1	Will this non-coal (industrial minerals) mining project involve the crushing and screening of non-coal minerals other than sand and gravel?	Yes		No
2.2	Will this non-coal (industrial minerals) mining project involve the crushing and/or screening of sand and gravel with the exception of wet sand and gravel operations (screening only) and dry sand and gravel operations with a capacity of less than 150 tons/hour of unconsolidated materials?	Yes		No

2.3	Will this non-coal (industrial minerals) mining project involve the construction, operation and/or modification of a portable non- metallic (i.e., non-coal) minerals processing plant under the authority of the General Permit for Portable Non-metallic Mineral Processing Plants (i.e., BAQ-PGPA/GP-3)? For this non-coal (industrial minerals) mining project, will sewage	Yes		No
	treatment facilities be constructed and treated waste water discharged to surface waters?			
2.5	Will this non-coal (industrial minerals) mining project involve the construction of a permanent impoundment meeting one or more of the following criteria: (1) a contributory drainage area exceeding 100 acres; (2) a depth of water measured by the upstream toe of the dam at maximum storage elevation exceeding 15 feet; (3) an impounding capacity at maximum storage elevation exceeding 50 acre-feet?	Yes		Νο
3.0	Will your project, activity, or authorization have anything to do with a well related to oil or gas production, have construction within 200 feet of, affect an oil or gas well, involve the waste from such a well, or string power lines above an oil or gas well? If "Yes", respond to 3.1-3.3. If "No", skip to Question 4.0.	Yes		No
3.1	Does the oil- or gas-related project involve any of the following: placement of fill, excavation within or placement of a structure, located in, along, across or projecting into a watercourse, floodway or body of water (including wetlands)?	Yes	\boxtimes	No
3.2	Will the oil- or gas-related project involve discharge of industrial wastewater or stormwater to a dry swale, surface water, ground water or an existing sanitary sewer system or storm water system? If "Yes", discuss in <i>Project Description</i> .	Yes		No
3.3	Will the oil- or gas-related project involve the construction and operation of industrial waste treatment facilities?	Yes	\boxtimes	No
4.0	Will the project involve a construction activity that results in earthdisturbance?If "Yes", specify the total disturbed acreage.4.0.1Total Disturbed Acreage	Yes	\boxtimes	No
	4.0.2 Will the project discharge or drain to a special protection water (EV or HQ) or an EV wetland?	Yes		No
	4.0.3 Will the project involve a construction activity that results in earth disturbance in the area of the earth disturbance that are contaminated at levels exceeding residential or non-residential medium-specific concentrations (MSCs) in 25 Pa. Code Chapter 250 at residential or non- residential construction sites, respectively?	Yes		No
5.0	Does the project involve any of the following: water obstruction and/or encroachment, wetland impacts, or floodplain project by the Commonwealth/political subdivision or public utility? If "Yes", respond to 5.1-5.3. If "No", skip to Question 6.0.	Yes		No
5.1	Water Obstruction and Encroachment Projects – Does the project involve any of the following: placement of fill, excavation within or placement of a structure, located in, along, across or projecting into a watercourse, floodway or body of water?	Yes		No
5.2	Wetland Impacts – Does the project involve any of the following: placement of fill, excavation within or placement of a structure, located in, along, across or projecting into a wetland?	Yes		No
5.3	Floodplain Projects by the Commonwealth, a Political Subdivision of the Commonwealth or a Public Utility – Does the project involve any of the following: placement of fill, excavation within or placement of a structure, located in, along, across or projecting into a floodplain?	Yes		No
5.4	Is your project an interstate transmission natural gas pipeline?	Yes		No

5.5	Does your project consist of linear construction activities which result in earth disturbance in two or more DEP regions AND three or more counties?		Yes		No
5.6	Does your project utilize Floodplain Restoration as a best management practice for Post Construction Stormwater Management?		Yes		No
5.7	Does your project utilize Class V Gravity / Injection Wells as a best management practice for Post Construction Stormwater Management?		Yes		No
6.0	Will the project involve discharge of construction related stormwater to a dry swale, surface water, ground water or separate storm water system?		Yes	\boxtimes	No
6.1	Will the project involve discharge of industrial waste stormwater or wastewater from an industrial activity or sewage to a dry swale, surface water, ground water or an existing sanitary sewer system or separate storm water system?		Yes		No
7.0	Will the project involve the construction and operation of industrial waste treatment facilities?		Yes	\boxtimes	No
8.0	 Will the project involve construction of sewage treatment facilities, sanitary sewers, or sewage pumping stations? If "Yes", indicate estimated proposed flow (gal/day). Also, discuss the sanitary sewer pipe sizes and the number of pumping stations/treatment facilities/name of downstream sewage facilities in the <i>Project Description</i>, where applicable. 8.0.1 Estimated Proposed Flow (gal/day) 		Yes		No
9.0	Will the project involve the subdivision of land, or the generation of 800 gpd or more of sewage on an existing parcel of land or the generation of an additional 400 gpd of sewage on an already- developed parcel, or the generation of 800 gpd or more of industrial wastewater that would be discharged to an existing sanitary sewer system?		Yes		No
	9.0.1 Was Act 537 sewage facilities planning submitted and approved by DEP? If "Yes" attach the approval letter. Approval required prior to 105/NPDES approval.		Yes		No
10.0	Is this project for the beneficial use of biosolids for land application within Pennsylvania? If "Yes" indicate how much (i.e. gallons or dry tons per year). 10.0.1 Gallons Per Year (residential septage) 10.0.2 Dry Tons Per Year (biosolids)		Yes		No
11.0	Does the project involve construction, modification or removal of a dam? If "Yes", identify the dam. 11.0.1 Dam Name		Yes		No
12.0	Will the project interfere with the flow from, or otherwise impact, adam? If "Yes", identify the dam.12.0.1Dam Name		Yes		No
13.0	Will the project involve operations (excluding during the construction period) that produce air emissions (i.e., NOX, VOC, etc.)?	\boxtimes	Yes		No
	13.0.1 If "Yes", is the operation subject to the agricultural exemption in 35 P.S. § 4004.1?		Yes		No
	 13.0.2 If the answer to 13.0.1 is "No", identify each type of emission followed by the estimated amount of that emission. Enter all types & amounts of See Emission Estimates Attached emissions; separate each set with semicolons. 				

14.0	Does the project include the construction or modification of a drinking water supply to serve 15 or more connections or 25 or more people, at least 60 days out of the year? If "Yes", check all proposed sub-facilities. 14.0.1 Number of Persons Served		Yes		No
	14.0.2 Number of Employee/Guests				
	14.0.3 Number of Connections				
	14.0.4 Sub-Fac: Distribution System		Yes		No
	14.0.5 Sub-Fac: Water Treatment Plant		Yes		No
	14.0.6 Sub-Fac: Source		Yes		No
	14.0.7 Sub-Fac: Pump Station	Π	Yes	Π	No
	14.0.8 Sub Fac: Transmission Main	Π	Yes	Π	No
	14.0.9 Sub-Fac: Storage Facility	П	Yes	П	No
15.0	Will your project include infiltration of storm water or waste water		Yes		No
	to ground water within one-half mile of a public water supply well.				
	spring or infiltration gallery?				
16.0	Is your project to be served by an existing public water supply? If		Yes	\boxtimes	No
1010	"Yes" indicate name of supplier and attach letter from supplier stating				
	that it will serve the project				
	16.0.1 Supplier's Name				
	16.0.2 Letter of Approval from Supplier is Attached		Yes		Νο
17 0	Will this project be served by on-lot drinking water wells?		Yes		No
18.0	Will this project be served by on let drinking water wens:		Yes		No
10.0	withdrawal from a river stream spring lake well or other water		100		
	bod(ies)? If "Yes" reference Safe Drinking Water Program				
	18.0.1 Source Name				
10.0	Will the construction or operation of this project involve treatment		Vec		No
19.0	storage reuse or disposal of waste? If "Ves" indicate what type (i.e.		163		NO
	bazardous municipal (including infactious & chamatharapoutic)				
	residual) and the amount to be treated stored to used or disposed				
	1901 Tuno & Amount				
20.0	Will your project involve the removal of coal minerals		Ves		No
20.0	contaminated media or solid waste as part of any earth disturbance		163		NO
	activities?				
21.0	Does your project involve installation of a field constructed		Yes	\square	No
21.0	underground storage tank? If "Ves" list each Substance & its		100		
	Capacity Note: Applicant may need a Storage Tank Site Specific				
	Installation Permit				
	21.0.1 Enter all substances &				
	canacity of each: separate				
	each set with semicolons				
22.0	Does your project involve installation of an aboveground storage		Yes	\boxtimes	No
	tank greater than 21,000 gallons capacity at an existing facility? If				
	"Yes", list each Substance & its Capacity, Note: Applicant may need a				
	Storage Tank Site Specific Installation Permit.				
	22.0.1 Enter all substances &				
	capacity of each: separate				
	each set with semicolons.				
23.0	Does your project involve installation of a tank greater than		Yes	\boxtimes	No
	1,100 gallons which will contain a highly hazardous substance as				
	defined in DEP's Regulated Substances List. 2570-BK-DEP2724? If				
	"Yes", list each Substance & its Capacity. Note: Applicant may need a				
	Storage Tank Site Specific Installation Permit.				
	23.0.1 Enter all substances &				
	capacity of each; separate				
	each set with semicolons.				

24.0	Does your project involve installation of a storage tank at a new		Yes	\boxtimes	No
	facility with a total AST capacity greater than 21,000 gallons? If				
	"Yes", list each Substance & its Capacity. Note: Applicant may need a				
	Storage Tank Site Specific Installation Permit.				
	24.0.1 Enter all substances &				
	capacity of each; separate				
	each set with semicolons.				
	NOTE: If the project includes the installation of a regulated storage tank	system	, including d	iesel e	mergency
	generator systems, the project may require the use of a Department Cen	tified T	ank Handler	For a	full list of
	regulated storage tanks and substances, please go to www.dep.pa.gov s	earch te	erm storage	tanks	
25.0	Will the intended activity involve the use of a radiation source?		Yes	\boxtimes	No
	CERTIFICATION				

I certify that I have the authority to submit this application on behalf of the applicant named herein and that the information provided in this application is true and correct to the best of my knowledge and information.

For applicants supplying an EIN number: I am applying for a permit or authorization from the Pennsylvania Department of Environmental Protection (DEP). As part of this application, I will provide DEP with an accurate EIN number for the applicant entity. By filing this application with DEP, I hereby authorize DEP to confirm the accuracy of the EIN number provided with the Pennsylvania Department of Revenue. As applicant, I further consent to the Department of Revenue discussing the same with DEP prior to issuance of the Commonwealth permit or authorization.

Sam Schupbach Type or Print Name VP Operations Processing 6/29/2022 Date Signature Title

Plan Approval Application Forms



COMMONWEALTH OF PENNSYLVANIA DEPARTMENT OF ENVIRONMENTAL PROTECTION BUREAU OF AIR QUALITY

PROCESSES

Application for Plan Approval to Construct, Modify or Reactivate an Air Contamination Source and/or Install an Air Cleaning Device

This application must be submitted with the General Information Form (GIF).

Before completing this form, read the instructions provided for the form.

Section A - Fac	ility Name, Checkli	ist And Certification
Organization Name or Registered Fictitious Na	me/Facility Name: <u>Mark</u>	kWest Liberty Midstream & Resources, LLC
Type of Review required and Fees:		
 Source which is not subject to NSPS, Source requiring approval under NSP Source requiring approval under NSR Source requiring the establishment of Source requiring approval under PSD 	NESHAPs, MACT, NSF S or NESHAPS or both regulations: a MACT limitation:	R and PSD:\$::\$7,500 \$\$ \$\$\$
	Applicant's Check	klist
Check the following list to n	nake sure that all the r	required documents are included.
⊠ General Information Form (GIF)		
Processes Plan Approval Applica	tion	
Compliance Review Form or pro facilities submitting on a periodic ba	ovide reference of mos sis:	est recently submitted compliance review form for
☑ Copy and Proof of County and Ma	unicipal Notifications	
🛛 Permit Fees		
Addendum A: Source Applicable F	Requirements (only app	licable to existing Title V facility)
Certification of Truth, Accu	racy and Complete	eness by a Responsible Official
I, Sam Schupbach	, certify under penal	lty of law in 18 Pa. C. S. A. §4904, and
35 P.S. §4009(b) (2) that based on information	and belief formed afte	r reasonable inquiry, the statements and information
in this application are true, accurate and compl	ete.	
S. Salial	D :	1/20/2022
(Signature):	Date	
Name (Print): <u>Sam Schupbach</u>		e: VP G&P Operations East
	OFFICIAL USE ONI	LY
Application No.	Unit ID	Site ID
DEP Client ID #:	APS. ID	AUTH. ID
Date Received	Date Assigned	Reviewed By
Date of 1 st Technical Deficiency Comments:	Date	e of 2 ^{na} Technical Deficiency

	Se	ection B - Pro	cesses Informat	on	
1. Source Inform	mation				
Source Description Harmon Creek Cryo the facility will includ added components However, maintena	(give type, use, raw n o II (260 MMSCFD) wi de maintenance blowd , and one (1) new 500 nce blowdowns and F	naterials, product ill include one (1) downs from three 0-gallon methanol 2SVs from Harmo	t, etc). Attach addition new 19.62 MMBtu/h (3) new electric-drive I tank. The existing pl on Creek Cryo II will b	al sheets as r heater. Poter on compresso ant flare PTE e controlled b	necessary. ntial de minimis increases at rs, fugitive emissions from will remain unchanged. y the process flare.
Manufacturer		Model N	lo.	Numb	er of Sources
Source Designation Regen Heater	1	Maximu 19.62 M	m Capacity IMBtu/r (HHV)	Rated 16.21	Capacity MMBtu/hr
Type of Material Pro 16.21 MMBtu/hr	ocessed				
Maximum Operatii	ng Schedule				
Hours/Day 24	Days/Wee 7	ek	Days/Year 365 bottlenecks or volunt	ary restriction	Hours/Year 8760 s to limit PTE)
		steu, il ally (e.g.,			s to minit F T L)
Per Hour	Per Day 260 MMS	CF	Per Week		Per Year
Operating Schedu	le				
Hours/Day 24	Days/Wee 7	łK	Days/Year 365		Hours/Year 8760
Seasonal variations	(Months) From		to	·	
	,				
2. Fuel	Quantity			% Ash	
Туре	Hourly	Annually	Sulfur	(Weight)	BTU Content
Oil Number 	GPH @ 60°F	X 10³ Gal	% by wt		Btu/Gal. & Lbs./Gal. @ 60 °F
Oil Number	GPH @ 60°F	X 10³ Gal	% by wt		Btu/Gal. & Lbs./Gal. @ 60 °F
Natural Gas	SCFH	0.017 X 10 ⁶ SCF	grain/100 SCF		1153 Btu/SCF
Gas (other)	SCFH	X 10 ⁶ SCF	grain/100 SCF		Btu/SCF
Coal	TPH	Tons	% by wt		Btu/lb
Other *					
*Note: Describe an	d furnish information	separately for oth	ner fuels in Addendun	ו B.	•

Section B - Processes Information (Continued)						
3. Burner						
Manufacturer Tulsa Heaters	Type and Mo H-2711	del No.		Nu 1	mber of Burners	
Cryo II Regeneration Heater						
Rated Capacity 16.21 MMBtu/hr	N 1	laximum C 9.62 MMBt	apacity tu/hr			
4. Process Storage Vessels						
A. For Liquids: (New Source)						
Name of material stored Methanol						
Tank I.D. No.	Manufacturer			Date Installed		
TK-1102	Exterran			Upon Approva		
Design Pressure 16 oz/in2		Capacity 500	(gallons/M	leter ³)		
Type of relief device (pressure set vent/ N/A	conservation vent/en	nergency v	ent/open v	ent)		
Relief valve/vent set pressure (psig) N/A		Vapor pro N/A	ess. of liqu	id at storage ten	np. (psia/kPa)	
Type of Roof: Describe: None – Horizontal tank						
Total Throughput Per Year 3,000 gal		Number of fills per day (fill/day): Filling Rate (gal./min.): Duration of fill hr /fill):				
B. For Solids – Not Applicable				,		
Type: Silo Storage Bin Othe	r, Describe	Name of	Material S	tored		
Silo/Storage Bin I.D. No.	Manufacturer			Date Installed		
State whether the material will be stored	l in loose or bags in s	silos	Capacity	(Tons)		
Turn over per year in tons			Turn ovei	⁻ per day in tons		
Describe fugitive dust control system for	loading and handlin	g operatior	าร			
Describe material handling system						
5. Request for Confidentiality						
Do you request any information on this a If yes, include justification for confidentia	application to be trea ality. Place such info	ted as "Co rmation on	nfidential"? separate p	Yes I Yes ages marked " c	No confidential".	

Section B - Processes Information (Continued)

6. Miscellaneous Information

Attach flow diagram of process giving all (gaseous, liquid and solid) flow rates. Also, list all raw materials charged to process equipment, and the amounts charged (tons/hour, etc.) at rated capacity (give maximum, minimum and average charges describing fully expected variations in production rates). Indicate (on diagram) all points where contaminants are controlled (location of water sprays, collection hoods, or other pickup points, etc.). Describe collection hoods location, design, airflow and capture efficiency. Describe any restriction requested and how it will be monitored.

See PFD appended.

Describe fully the facilities provided to monitor and to record process operating conditions, which may affect the emission of air contaminants. Show that they are reasonable and adequate.

A fuel usage meter will be installed to monitor fuel consumption by the heater (032).

Describe each proposed modification to an existing source.

Pigging frequency is expected to increase. However, the frequency is not anticipated to be greater than that included in the modification application submitted on 12/10/2020. Therefore, potential emission estimates will remain unchanged. Pigging emissions will be controlled by the plant flare.

The plant flare (C601), currently authorized under GP5-63-01011A, will control the proposed compressor maintenance blowdowns and emissions from pressure relief valves, where feasible. The potential-to-emit from the flare in the applications submitted on 6/12/2017 and 12/10/2020 included Cryo II and is not being increased under this application. However, the construction period for Cryo II has lapsed and requires authorization to construct. The basis for the potential emission estimates in the two previous applications will remain unchanged in this plan approval application.

Identify and describe all fugitive emission points, all relief and emergency valves and any by-pass stacks.

The potential emission estimates attached have accounted for fugitive emission points associated with the new equipment. Some pressure relief devices, where feasible, will be controlled by the plant flare.

Pumps are monitored via weekly inspections and monthly Method 21. MPLX conducts a quarterly LDAR program using a gas leak detector approved for Method 21 and/or an OGI camera. In addition, Harmon Creek operators conduct daily AVO inspections.

Describe how emissions will be minimized especially during start up, shut down, process upsets and/or disruptions.

Consistent with the 2018 Consent Decree (CD), pigging equipment at Harmon Creek is equipped with pig ramps and grounded steel receptacles that are covered when not in use, and vapors from depressurizing pigging barrels are routed to the plant flare. The CD requires high pressure pigging equipment to be connected to a low pressure gathering line where commercially reasonable and technically feasible. The connection of the high pressure launcher to a low pressure line would require MPLX to use more than 100 feet of piping and connect to a line located outside the fence line of the facility. Thus, per the CD, jumper lines at Harmon Creek are not commercially reasonable and technically feasible.

When feasible, emissions from compressor blowdowns and facility outages will be routed to the plant flare.

Anticipated Milestones:

- i. Expected commencement date of construction/reconstruction/installation: January 2
- ii. Expected completion date of construction/reconstruction/installation:iii. Anticipated date of start-up:
- January 2023 January 2024 January 2024

Section C - Air Cleaning Device								
1. Precontrol Emissions* - See Emission Calculations Attached								
		Maximum	Emission Rate	1	Calculation/			
Pollutant	Specify Units	Pounds/Hour	Hours/Year	Tons/Year	Estimation Method			
PM								
PM10								
SOx								
CO								
NOx								
VOC								
Others: (e.g., HAPs)								
* These emissions mu schedule for maximu values were determin	st be calculated bas m limits or restricted red. Attach calculatio	ed on the request I hours of operations.	ed operating schedule on and/or restricted thr	e and/or process rate oughput. Describe h	e, e.g., operating ow the emission			
2. Gas Cooling – N	/A							
Water quenching	Yes 🗌 No	Water injection ra	te	GPM				
Radiation and convectio	on cooling		Air dilution	Yes 🗌 No FM				
Forced Draft 🗌 Yes	No		Water cooled duct wor	k 🗌 Yes 🗌	No			
Other								
Inlet Volume	ACFM		Outlet Volume	ACFM				
@°F	% Moisture		@°F	% Moisture				
Describe the system in	detail.							

Section C - Air Cleaning Device (Continued)							
12. Flares (Existing Source)							
Equipment Specification	S						
Manufacturer		Type 🗌 Elev	vated flare	nd flare	Model No.		
John Zink		Oth	er <u>Air Assisted</u>	Describe	EEF Series		
Design Volume (SCFM)		Dimensions of s	tack (ft.)				
Design Volumes provided	by	Diameter 6'11"	Height <u>199</u>				
scenarios.	a on dillerent						
Facility Potential Volume:	100 mmscf/yr						
Residence time (sec.) and	outlet	Turn down ratio		Burner details			
temperature (°F)				Waste gas			
Describe the flare design (flare with a sketch.	air/steam-assi	sted or nonassiste	d), essential auxiliaries ir	ncluding pilot flame m	onitor of proposed		
Stable in winds up to a ve tip windshield, ignition an thermowells for thermoco- flare. The motors driving the wide range of rotational sp	Stable in winds up to a velocity of 160 mph in all positions around the flare tip, the WindPROOF Pilot consists of a tip and tip windshield, ignition and fuel piping, venturi mixer, strainer, and a mixer windshield. Also included are two integral thermowells for thermocouple pilot detection. Two blowers to supply low pressure air are provided with the air assisted flare. The motors driving these blowers are designed to operate with a Variable Frequency Drive (VFD). The VFD allows a wide range of rotational speeds (twoically from 10 to 100%)						
Describe the operation of t	he flare's igniti	on system.					
The Zeus Electric Spark Ig ignites a small slip stream generated at the probe tra The Zeus ignitor control bo approximately once every	nitor delivers a of gas/air mixtu vels a short dis ox located in a 8 seconds.	a spark at the end ure taken from the stance from the en panel at grade use	of a probe mounted on th main pilot supply above d of the probe to the pilot es a capacitive discharge	ne Zeus equipped pilo the pilot mixer. The fl ignition hood where to generate a periodi	t. The spark ame front it lights the pilot. ic spark		
Describe the provisions to	introduce auxi	liary fuel to the flar	e.				
None needed.							
Operation Parameters							
Detailed composition of th	e waste gas	Heat content	Exit velocity				
Conservatively assumes f See detailed emission cal attached.	acility inlet. culations	1413.78	Maximum velocity calculated base manufacturer provided design scent flowrate is 83.3 ft/s				
Maximum and average ga	s flow burned (ACFM)	Operating temperature (°F)			
Maximum flow rate based design scenarios is 558,50	on manufactur)0 lb/hr.	er provided	Varies				
Facility Potential Volume:	100 mmscf/yr						
Describe the warning/alarr	n system that p	protects against op	peration when unit is not	meeting design requir	ements.		
Alarms are set to trigger w trigger alarms are determined	hen specific co ned based on (onditions are met s Cause and Effect o	such as the absence of a control documents.	pilot flame. The cond	itions which		
Emissions Data							
Pollutant	I	Inlet	Outlet	Removal Ef	ficiency (%)		
VOC	673.04 tpy		13.46 tpy	98%			
HAP	48.82 tpy		0.98 tpy	98%			

Section C - Air Cleaning Device (Continued)								
13. Other Control Equi	pment – <mark>N/A</mark>							
Equipment Specification	IS	1						
Manufacturer		Туре		Model No.				
Design Volume (SCFM)			Capacity					
Describe pH monitoring a	nd pH adjustme	nt, if any.						
Indicate the liquid flow rate	Indicate the liquid flow rate and describe equipment provided to measure pressure drop and flow rate, if any.							
Attach efficiency curve and	d/or other efficie	ency information.						
Attach any additional date	including auxili	ary equipment an	d operation details to tho	roughly evaluate the control equipment.				
Operation Parameters								
Volume of gas handled								
AC	CFM @	°F	% N	loisture				
Describe fully giving important parameters and method of operation.								
Describe the warning/alarm system that protects against operation when unit is not meeting design requirements.								
Emissions Data			1	I				
Pollutant	I	nlet	Outlet	Removal Efficiency (%)				

	Section C - Air Cleaning Device (Continued)									
14.	Costs									
Indic	ate cost associated wit	h air cleaning device	and its operating cost	(attach documentation	ı if necessary)					
The	plant flare is an existing	g source.								
	Device	Direct Cost	Indirect Cost	Total Cost	Annual Operating Cost					

15. Miscellaneous

Describe in detail the removal, handling and disposal of dust, effluent, etc. from the air cleaning device including proposed methods of controlling fugitive emissions.

N/A

Attach manufacturer's performance guarantees and/or warranties for each of the major components of the control system (or complete system).

The existing plant flare has guaranteed destruction efficiency of 98%

Attach the maintenance schedule for the control equipment and any part of the process equipment that if in disrepair would increase air contaminant emissions.

	Section D - Additional Information							
Wi the	Will the construction, modification, etc. of the sources covered by this application increase emissions from other sources at the facility? If so, describe and quantify.							
No	No. All sources with the potential to increase in emissions have been included in this application.							
lf t	If this project is subject to any one of the following, attach a demonstration to show compliance with applicable standards							
a.	Prevention of Significant Deterioration permit (PSD), 40 CFR 52?	☐ YES	⊠ NO					
b.	New Source Review (NSR), 25 Pa. Code Chapter 127, Subchapter E?	Tes 🗌	⊠ NO					
C.	New Source Performance Standards (NSPS), 40 CFR Part 60? (If Yes, which subpart) <u>OOOOa, Dc</u>	🛛 YES	□ NO					
d.	National Emissions Standards for Hazardous Air Pollutants (NESHAP), 40 CFR Part 61? (If Yes, which subpart)	☐ YES	⊠ NO					
e.	Maximum Achievable Control Technology (MACT) 40 CFR Part 63? (If Yes, which part)	☐ YES	⊠ NO					

Attach a demonstration showing that the emissions from any new sources will be the minimum attainable through the use of best available technology (BAT).

As requested by the Department, MPLX is including a BAT analysis for the addition of an enclosed combustor to control Harmon Creek Cryo II.

The existing flare at Harmon Creek has a destruction efficiency of at least 98%, which is equivalent to the destruction efficiency of the enclosed combustor. Thus, no emission reductions will result from operating an enclosed combustor to control Harmon Creek II maintenance blowdowns and PSVs, demonstrating that the existing flare meets BAT.

Additional pilot and purge gas would be required to operate an enclosed combustor, increasing emissions at the facility. The PTE increase is summarized in the BAT Cost Table below. The basis for the enclosed combustor emission estimates is provided on page 23 of the application.

The direct cost for the enclosed combustor is provided in the table on page 24 of the application. Indirect costs have been estimated based on costs for similar projects.

As demonstrated in this section, the installation and operation of an enclosed combustor would increase emissions at Harmon Creek and thus, is not economically reasonable.

Best Available Technology Costs									
Device	Direct Cost	Indirect Cost	Total Cost	Annual Operating Cost	PTE Change (TPY)				
Enclosed Combustor	\$10,000,000	\$10,000,000	\$20,000,000		VOC: +0.01 CO: +2.04 NOx: +0.45 PM: +0.05 CO2: +771.55 CH4: +4.90				

Provide emission increases and decreases in allowable (or potential) and actual emissions within the last five (5) years for applicable PSD pollutant(s) if the facility is an existing major facility (PSD purposes).

Not Applicable

MarkWest Liberty Midstream & Resources, L.L.C. Harmon Creek Gas Plant

Enclosed Combustor Pilot and Purge Emission Estimates

Source Designation:	
Manufacturer:	Zeeco
Operating Hours: (hr/yr)	8,760
Pilot + Purge Gas Heat Input (MMBtu/hr)	1.503
Pilot + Purge Gas Annual Fuel Use (mmscf/yr)	12.439
Pilot Fuel Consumption (mmscf/hr):	1.10E-03
Purge Fuel Consumption (mmscf/hr):	3.20E-04
Fuel HHV (Btu/scf)	1,059

Total Emissions

Pollutant	Emission Factor (lb/MMBtu)	lb/hr	tpy
VOC		0.00	0.01
HAP		0.00	0.00
NO _X	0.068	0.10	0.45
CO	0.31	0.47	2.04
SO ₂	0.0006	0.00	0.00
PM Total	0.0075	0.01	0.05
PM Condensable	0.0056	0.01	0.04
PM ₁₀ (Filterable)	0.0019	0.00	0.01
PM _{2.5} (Filterable)	0.0019	0.00	0.01
CO ₂	117.05	176.15	771.55
CH_4	0.002	1.12	4.90
N ₂ O	0.0002	0.00	0.00

^a The NOx and CO emission factors are from AP-42 Section 13.5 "Industrial Flares" Table 13.5-1.

^b Emission factors for GHG pollutants from 40 CFR Part 98, Subpart C. Tables C-1 and C-2.

^c The remaining factors are from AP-42 Section 1.4 "Natural Gas Combustion" Tables 1.4-1 and 1.4-2.

^d VOC and HAP emissions are based on mass balance.

PROCESS CONDITIONS											
		Deethan	izer Plant				Cryo Plant			Global	Plant Inlet
	PSV-251	PSV-155/156/157	PSV-456	PSV-458	PSV-422B	PSV-321	PSV-140/1/2	PSV-521 New	PSV-151/2/3/4D	Multiple	
Description	DeC2 Reboiler	Refrig Comp	C3+ Tank	Ethane Tank	DeC1 Surge Tank	A-321	Refrig Comp	Demethanizer LCV	Residue Comp	Dowor Failura	Slug Catcher
Case	Reflux Failure	Blocked Outlet	Fire	Fire	Fire	Control Failure	Blocked Outlet	Bypass Failure	Blocked Outlet	Power Failure	Fire
PSV Set Pressure	550	350	550	550	550	540	350	550	1310		1440
Flow Rate (lb/hr)	528,094	754,400	843,008	415,642	296,598	711,364	754,400	663,115	1,117,000	1,244,327	732,000
Molecular Weight	48.1	44.1	50.3	29.9	50.87	21.76	44.1	20.88	18.8	21.97	39.46
Lower Heating Value (Btu/SCF)	2515	2317	2624	1610	2651	1187	2317	1149	1039	1205	2068
Temperature @ Inlet (°F)	265	142	60	-127	275	108	142	-38.6	186	58.4	400
Smokeless Requirements (%)	100	100	0	0	100	100	100	0	0	0	0
Allowable pressure @ Inlet (psig)	Vendor	Vendor	Vendor	Vendor	Vendor	Vendor	Vendor	Vendor	Vendor	Vendor	Vendor
Composition (mol%)											
C1	0.00	0.00	0.00	1.97	0.00	74.31	0.00	76.43	81.49	73.06	38.35
C2	2.18	1.00	1.38	97.63	1.32	15.54	1.00	15.32	16.95	16.45	18.10
C3	73.41	98.00	65.54	0.40	62.98	5.87	98.00	5.27	0.89	6.23	13.79
i-C4	5.56	1.00	6.39	0.00	6.75	0.64	1.00	0.50	0.03	0.69	2.68
n-C4	13.51	0.00	16.96	0.00	18.23	1.79	0.00	1.31	0.05	1.91	9.03
C5+	5.34	0.00	9.73	0.00	10.22	1.31	0.00	0.61	0.00	1.14	17.79
H2S	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
CO	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
H2	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
N2	0.00	0.00	0.00	0.00	0.50	0.39	0.00	0.40	0.43	0.38	0.14
02	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
C6H6	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
NH3	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
Others-CO2	0.00	0.00	0.00	0.00	0.00	0.15	0.00	0.15	0.16	0.15	0.12
ZEECO NOTES BELOW											
No Units	1	1	1	1	1	1	1	1	2	2	1
Chamber Diameter (FT)		74	78			74	74		68	72	74
Chamber Height (FT)		124	124			122	124		115	113	120
ZEEDD Overall Height (FT)		152	154			150	152		140	140	148
WF Diameter (FT)		105	110			105	105		96	102	105
Budgetary Price		\$ 5,700,000.00	\$ 6,500,000.00			\$ 5,700,000.00	\$ 5,700,000.00		\$ 9,000,000.00	\$ 10,000,000.00	\$ 5,700,000.00
Delivery (Weeks)		58	62			58	58		66	66	58

Section D - Additional Information (Continued) - Not Applicable

Indicate emission increases and decreases in tons per year (tpy), for volatile organic compounds (VOCs) and nitrogen oxides (NOx) for NSR applicability since January 1, 1991 or other applicable dates (see other applicable dates in instructions). The emissions increases include all emissions including stack, fugitive, material transfer, other emission generating activities, quantifiable emissions from exempted source(s), etc.

		Indicate Yes		VO	Cs	N	Ox
		or No if		Emission			
		emission		increases	Creditable	Emission	Creditable
		increases and		in	emission	increases	emission
		decreases		potential	decreases	in	decreases
Permit	5 /	were used		to emit	in actual	potential	in actual
number	Date	previously for			emissions	to emit	emissions
(if applicable)	issued	netting	Source I. D. or Name	(tpy)	(tpy)	(tpy)	(tpy)

If the source is subject to 25 Pa. Code Chapter 127, Subchapter E, New Source Review requirements,

a. Identify Emission Reduction Credits (ERCs) for emission offsets or demonstrate ability to obtain suitable ERCs for emission offsets.

b. Provide a demonstration that the lowest achievable emission rate (LAER) control techniques will be employed (if applicable).

c. Provide an analysis of alternate sites, sizes, production processes and environmental control techniques demonstrating that the benefits of the proposed source outweigh the environmental and social costs (if applicable).

Attach calculations and any additional information necessary to thoroughly evaluate compliance with all the applicable requirements of Article III and applicable requirements of the Clean Air Act adopted thereunder The Department may request additional information to evaluate the application such as a standby plan, a plan for air pollution emergencies, air quality modeling, etc.

	S	ection E - Compliance Dem	onstration			
Note:	Complete this section if sour	ce is not a Title V facility. Title V f	acilities must complete Addendum A.			
Metho	d of Compliance Type: Check	all that apply and complete all appl	ropriate sections below			
\square	Monitoring	ting 🛛 🖂 Repo	orting			
\boxtimes	Recordkeeping Work Practice Standard					
Monito	oring: Regen Heater					
a.	Monitoring device type (Param	eter, CEM, etc): Fuel gas mete	er			
b.	Monitoring device location:	Regen heater (032) fuel gas heade	er			
C.	Describe all parameters being	monitored along with the frequency	and duration of monitoring each parameter:			
	Daily fuel das usade					
Monito	oring: Fugitive Components					
a.	Monitoring device type (Param	eter, CEM, etc): Method 21 or	OGI			
b.	Monitoring device location:	Portable				
C.	Describe all parameters being	monitored along with the frequency	and duration of monitoring each parameter:			
	Component Type	Monitoring Frequency	Detection Level (PPMV)			
	Compressor	Quarterly/Annually	10.000 (OGI) / 500			
	Connector	Quarterly/Annually	10,000 (OGI) / 500			
	Pressure Relief	Quarterly	500			
	Valve	Quarterly	500			
	Pump	Monthly	2,000			
Deeer	dire e nimer					
Record	akeeping: aariba what paramatara will ba r	approved and the reporting frequence				
De	scribe what parameters will be r	ecolded and the recording frequenc	cy.			
Re	gen Healer - Dally luer usage					
Reporting:						
a.	Describe what is to be reported	and frequency of reporting:				
	Regen Heater – Date of const	ruction (within 30 days) and startu	p (within 15 days) notifications			
	Fugitives - Semiannual reports	s per 40 CFR § 60.5422a				
b.	Reporting start date: Fugitives	- 6 months after the initial startup da	ate			

Section F - Flue and Air Contaminant Emission							
1. Estimated Atmos	pheric Emiss	ions*					
		Max	timum emiss	sion rate			
Pollutant	specify u (lb/mms (lb/mmbt	nits cf) :u)*	lbs/hr		tons/yr.	E	Calculation/ Estimation Method
PM	8.59	0.1	46	0.64	0	AP-4	42
PM10	2.15	0.0	37	0.16	0	AP-4	42
SO _x	0.68	0.012 0.05		1	AP-4	42	
СО	0.04*	0.7	85	3.43	8	Man	ufacturer Guarantee
NOx	0.04*	0.7	85	3.43	8	Man	ufacturer Guarantee
VOC	0.019*	0.3	73	1.63	3	Man	ufacturer Guarantee
HAPs	2.135	0.0	36	0.15	9	AP-4	42
* These emissions must schedule for maximum values were determine	* These emissions must be calculated based on the requested operating schedule and/or process rate e.g., operating schedule for maximum limits or restricted hours of operation and /or restricted throughput. Describe how the emission values were determined. Attach calculations.						
2. Stack and Exhaus	ster						
Stack Designation/Numl	ber S032						
List Source(s) or source 032	ID exhausted	to this stac	k:	% of flow exh	austed to sta	ick: 100	
Stack height above grad Grade elevation (ft.) App	le (ft.) 20 prox 1170	Sta 2.5	ack diameter	(ft) or Outlet	duct area (so	q. ft.)	f. Weather Cap
Distance of discharge to	nearest prop	erty line (ft.)	. Locate on t	opographic n	nap.		
>500							
Does stack height meet Yes	Good Enginee	ring Practice	e (GEP)?				
If modeling (estimating) and other obstructions. I	of ambient ai N/A	r quality imp	pacts is need	led, attach a	site plan wit	h buildings	and their dimensions
Location of stac Latitude/Longitu	ck** ude		Latitude			Long	gitude
Point of Origi	n	Degrees	Minutes	Seconds	Degrees	Minutes	Seconds
Approximate Location of	Cryo II	40	24	15	80	21	31
Stack exhaust Volume <u>15,796</u> lb/h	Stack exhaustVolume 15,796Ib/hrTemperature 461 °FMoisture N/A %						
Indicate on an attached sheet the location of sampling ports with respect to exhaust fan, breeching, etc. Give all necessary dimensions. N/A							
Exhauster (attach fan cu	rves)		in. of	water		HP @	RPM.
** If the data and colle Application, provide th	** If the data and collection method codes differ from those provided on the General Information Form-Authorization Application, provide the additional detail required by that form on a separate form.						

Section G - Attachments

Number and list all attachments submitted with this application below:

- 1 General Information Form
- 2 Plan Approval Application Forms
- 3 Compliance Review Form
- 4 Proof of Municipal Notification
- 5 Process Flow Diagram
- 6 Detailed Emission Estimates, including Manufacturer Information and Gas Analyses
- 7 Supporting Documentation
- 8 Permitting Fees

Compliance Review Form



COMMONWEALTH OF PENNSYLVANIA DEPARTMENT OF ENVIRONMENTAL PROTECTION BUREAU OF AIR QUALITY

AIR POLLUTION CONTROL ACT COMPLIANCE REVIEW FORM

SECTION B. GENERAL INFORMATION REGARDING "APPLICANT"

If applicant is a corporation or a division or other unit of a corporation, provide the names, principal places of business, state of incorporation, and taxpayer ID numbers of all domestic and foreign parent corporations (including the ultimate parent corporation), and all domestic and foreign subsidiary corporations of the ultimate parent corporation with operations in Pennsylvania. Please include all corporate divisions or units, (whether incorporated or unincorporated) and privately held corporations. (A diagram of corporate relationships may be provided to illustrate corporate relationships.) Attach additional sheets as necessary.

Unit Name	Principal Places of Business	State of Incorporation	Taxpayer ID	Relationship to Applicant
No changes				

SECTION C. SPECIFIC INFORMATION REGARDING APPLICANT AND ITS "RELATED PARTIES"

Pennsylvania Facilities. List the name and location (mailing address, municipality, county), telephone number, and relationship to applicant (parent, subsidiary or general partner) of applicant and all Related Parties' places of business, and facilities in Pennsylvania. Attach additional sheets as necessary.

Unit Name	Street Address	County and Municipality	Telephone No.	Relationship to Applicant
No changes				

Provide the names and business addresses of all general partners of the applicant and parent and subsidiary corporations, if any.

Name	Business Address
MPLX, LP	200 E. Hardin Street, Findlay, OH 45840
MarkWest Energy Partners, L.P.	1515 Arapahoe St, Tower 1, Suite 1600, Denver, CO. 80016
MarkWest Liberty M&R, L.L.C.	1515 Arapahoe St, Tower 1, Suite 1600, Denver, CO. 80016
MarkWest Liberty Bluestone, L.L.C.	1515 Arapahoe St, Tower 1, Suite 1600, Denver, CO. 80202

List the names and business address of persons with overall management responsibility for the process being permitted (i.e. plant manager).

Name	Business Address
Brandon Belford, Region Manager - Gathering	4600 J. Barry Ct., Canonsburg, PA. 15317
Jonathan C. Jackson, VP Eastern Region G&P	4600 J. Barry Ct., Canonsburg, PA. 15317
Gregory S. Floerke, EVP & COO MPLX	1515 Arapahoe St, Tower 1, Suite 1600, Denver, CO. 80016
Sam Schupbach, VP Operations Processing	4600 J. Barry Ct., Canonsburg, PA. 15317

Plan Approvals or Operating Permits. List all plan approvals or operating permits issued by the Department or an approved local air pollution control agency under the APCA to the applicant or related parties that are currently in effect or have been in effect at any time 5 years prior to the date on which this form is notarized. This list shall include the plan approval and operating permit numbers, locations, issuance and expiration dates. Attach additional sheets as necessary.

Air Contamination Source	Plan Approval/ Operating Permit#	Location	Issuance Date	Expiration Date
Houston Gas Plant	PA-63-00936F	800 Western Ave	10/4/2012	4/2019 (Renewal Submitted 10/25/2018) (Plan Approval
				Submitted 4/27/2021)
Baker CS	GP5-63- 00960E/AG5-63- 00013A & GP9-63- 00960B	151 Baker Station Road	6/28/2021	6/28/2026
Brigich CS	GP5-63-00954C	340 Brigich Road	10/7/2010	10/7/2015 (SOOP Submitted 8/31/2020)
Carpenter CS	GP5-63-00987A	265 Old National Pike	11/10/2014	10/31/2019 (Renewal Submitted 10/1/2019)
Down Homes CS	GP5-63-1009A	2037 Sunnyhill Road	5/16/2017	5/16/2022
Dryer CS	SOOP-63-00942	819 Scenic Drive	10/13/2020	10/13/2025
Fulton CS	SOOP-63-00937	103 Washington Ave	10/13/2020	10/13/2025
Godwin CS	SOOP-63-00934	2158 Henderson Ave	7/29/2021	7/29/2026
Harmon Creek Gas Plant	GP1-63-01011A GP5-63-01011A	Smith Township	1/17/2018	1/17/2023 (GP-5 Modification Submitted 12/10/2020)
Hoskins CS	GP5-63-00938B	4026 Buffalo Creek Road	8/22/2017	8/22/2022 (SOOP Submitted 9/2020)
Imperial-Cibus Ranch CS	GP5-63-00992A	2213 Quiksilver Rd. 2199 Quiksilver Rd.	3/22/2022	3/22/2027
Johnston CS	SOOP-63-00933	210 Johnston Hill Road	3/22/2022	3/22/2027
Lowry CS	GP5-63-00947B	100 Oakleaf Rd	6/22/2017	6/22/2022 (SOOP Submitted 9/2020)
McMichael CS	GP5-04-00747	1982 Hookstown Grade Rd.	11/19/2018	10/31/2023
Redd CS	GP5-63-00962	576 Redd Run Rd.	7/2/2021	7/2/2026
Shaw CS	GP5-63-00940C	492 Arden Mine Rd	8/18/2011	8/18/2016 (SOOP Submitted 9/2/2020)
Smith CS	SOOP-63-00962	320 Point Pleasant Rd	Issued: 12/2/2019 Modified: 3/22/2022	12/2/2024

2700-PM-AQ0004 Rev. 6/2006

Stewart CS	SOOP-63-00939	185 Avella Road	7/6/2021	7/6/2026
Three Brothers CS	GP5-63-00969 & Plan Approval 63- 00969A	858 Atlasburg Road	12/30/2011 (GP5) 8/27/2012 (PA)	12/30/2016 (GP5) 11/2/2015 (PA) (Extension submitted 10/15/2015) (SOOP Submitted 9/12/2018)
Tupta Day CS	GP5-63-00948E	200 Johnson Rd	1/10/2022	1/10/2027
Welling CS	GP5-00958A	165 Carlisle Rd	1/30/2015	1/30/2020 (Renewal Submitted 1/3/2020) (SOOP Submitted
				7/12/2021)
Sarsen Gas Plant	SOOP 10-00359	774 Prospect Rd.	12/03/2013	1/31/2024
Voll CS	SOOP-10-00367	318 Woodlands Rd. Evans City, PA	9/9/2020	8/31/2025
Trillith CS	GP5-10-370F	Southeast of intersection of Highway 79 an E Lancaster Rd	12/26/2018	11/30/2023
Royal Oak CS	SOOP 10-00390	961 Brownsdale Rd	12/16/2019	11/30/2024
Bluestone Gas Plant	TV-10-00368 PA-10-368G	440 Hartmann Rd.	2/20/2020 11/3/2020	1/31/2025 5/31/2022 (Administrative Modification Submitted to incorporate Plan App conditions into Title V permit).

Compliance Background. (Note: Copies of specific documents, if applicable, must be made available to the Department upon its request.) List all documented conduct of violations or enforcement actions identified by the Department pursuant to the APCA, regulations, terms and conditions of an operating permit or plan approval or order by applicant or any related party, using the following format grouped by source and location in reverse chronological order. Attach additional sheets as necessary. See the definition of "documented conduct" for further clarification. Unless specifically directed by the Department, deviations which have been previously reported to the Department in writing, relating to monitoring and reporting, need not be reported.

Date	Location	Plan Approval/ Operating Permit#	Nature of Documented Conduct	Type of Department Action	Status: Litigation Existing/Continuing or Corrected/Date	Dollar Amount Penalty
No change						\$
						\$
						\$
						\$
						\$
						\$

List all incidents of deviations of the APCA, regulations, terms and conditions of an operating permit or plan approval or order by applicant or any related party, using the following format grouped by source and location in reverse chronological order. This list must include items both currently known and unknown to the Department. Attach additional sheets as necessary. See the definition of "deviations" for further clarification.

Date	Location	Plan Approval/ Operating Permit#	Nature of Deviation	Incident Status: Litigation Existing/Continuing Or Corrected/Date
July 6, 2015	Various		Pig Launcher/Receiver Permitting	Signed Consent Decree with USEPA and PADEP. 7/19/2018
2016	Houston Plant and Other Gas Plants	PA-63-00936F	LDAR	Signed Consent Decree with USEPA and PADEP. 1/9/2019
March 23, 2017	Sarsen Gas Processing Plant	SOOP 10-00359	NSPS Subpart KKK	Signed Consent Decree with USEPA. 3/26/2017
August 28, 2020	Sarsen Gas Processing Plant	SOOP 10-00359	NSPS Subpart OOOO LDAR	Signed Consent Agreement and Final Order with USEPA. Filed 8/28/2020.

<u>CONTINUING OBLIGATION</u>. Applicant is under a continuing obligation to update this form using the Compliance Review Supplemental Form if any additional deviations occur between the date of submission and Department action on the application.

VERIFICATION STATEMENT

Subject to the penalties of Title 18 Pa.C.S. Section 4904 and 35 P.S. Section 4009(b)(2), I verify under penalty of law that I am authorized to make this verification on behalf of the Applicant/Permittee. I further verify that the information contained in this Compliance Review Form is true and complete to the best of my belief formed after reasonable inquiry. I further verify that reasonable procedures are in place to ensure that "documented conduct" and "deviations" as defined in 25 Pa Code Section 121.1 are identified and included in the information set forth in this, Compliance Review Form.

ally

Signature

6/29/2022 Date

Sam Schupbach

Name (Print or Type) VP Operations Processing

Title

Proof of Municipal Notifications


MarkWest Liberty Midstream and Resources, L.L.C. 1515 Arapahoe Street Tower 1, Suite 1600 Denver, CO 80202-2137 (800) 730-8388 (303) 925-9200 (303) 825-0902 Fax

June 28, 2022

Tracking Number: 1Z2E23250291333723

Township Supervisors Smith Township PO Box 94 Slovan, PA. 15078

Re: MarkWest Liberty Midstream and Resources, L.L.C. Harmon Creek Gas Plant Plan Approval Application

Dear Supervisors:

This letter is being sent to notify the Township Supervisors that MarkWest Liberty Midstream and Resources, L.L.C (MPLX) has applied to the Pennsylvania Department of Environmental Protection (PADEP) for an Air Quality Plan Approval for the Harmon Creek Gas Plant, located at 123 Point Pleasant Rd in Smith Township, Washington County, Pennsylvania.

MarkWest seeks to authorize the installation and operation of the following equipment at the facility:

- One (1) 260 mmscfd natural gas processing plant;
- One (1) regenerative heater rated at a maximum heat input of 19.62 MMBtu/hr;
- One (1) 500-gallon methanol storage tank;
- Three (3) electric-driven compressors and associated rod-packing venting; and
- Associated fugitive components.

De minimis emission increases associated with the existing pigging and truck loadout operations, in addition to emissions from maintenance blowdowns and some PSVs will be controlled by the existing process flare.

This notice is being provided in accordance with the requirements of 25 Pa. Code § 127.413 for municipal notification.

There is a 30-day comment period which begins upon receipt of this notice by the county. Anyone wishing to view this application may do so by making arrangements with:

Air Quality Program PADEP - Southwest Regional Office 400 Waterfront Drive Pittsburgh, PA. 15222 (412) 442-4000 If you have any questions about this application, please contact me at (412) 815-8886 or via email at <u>ajuarez@marathonpetroleum.com</u>.

Sincerely,

Alexandra M. Juary G&P Engineer I

cc: MarkWest file

Proof of Delivery

Dear Customer,

This notice serves as proof of delivery for the shipment listed below.

Tracking Number

1Z2E23250291333723

Service

UPS 2nd Day Air®

Shipped / Billed On

06/13/2022

Delivered On

06/29/2022 10:07 A.M.

Delivered To

SLOVAN, PA, US

Received By

KRENZLAK

Thank you for giving us this opportunity to serve you. Details are only available for shipments delivered within the last 120 days. Please print for your records if you require this information after 120 days.

Sincerely,

UPS

Tracking results provided by UPS: 06/29/2022 10:16 A.M. EST



MarkWest Liberty Midstream and Resources, L.L.C. 1515 Arapahoe Street Tower 1, Suite 1600 Denver, CO 80202-2137 (800) 730-8388 (303) 925-9200 (303) 825-0902 Fax

June 28, 2022

Tracking Number: 1Z2E23250395329229

Washington County Commissioners Courthouse Square 100 West Beau Street Suite 702 Washington, PA 15301

Re: MarkWest Liberty Midstream and Resources, L.L.C. Harmon Creek Gas Plant Plan Approval Application

Dear Commissioners:

This letter is being sent to notify the County Commissioners that MarkWest Liberty Midstream and Resources, L.L.C (MPLX) has applied to the Pennsylvania Department of Environmental Protection (PADEP) for an Air Quality Plan Approval for the Harmon Creek Gas Plant, located at 123 Point Pleasant Rd in Smith Township, Washington County, Pennsylvania.

MarkWest seeks to authorize the installation and operation of the following equipment at the facility:

- One (1) 260 mmscfd natural gas processing plant;
- One (1) regenerative heater rated at a maximum heat input of 19.62 MMBtu/hr;
- One (1) 500-gallon methanol storage tank;
- Three (3) electric-driven compressors and associated rod-packing venting; and
- Associated fugitive components.

De minimis emission increases associated with the existing pigging and truck loadout operations, in addition to emissions from maintenance blowdowns and some PSVs will be controlled by the existing process flare.

This notice is being provided in accordance with the requirements of 25 Pa. Code § 127.413 for municipal notification.

There is a 30-day comment period which begins upon receipt of this notice by the county. Anyone wishing to view this application may do so by making arrangements with:

Air Quality Program PADEP - Southwest Regional Office 400 Waterfront Drive Pittsburgh, PA. 15222 (412) 442-4000 If you have any questions about this application, please contact me at (412) 815-8886 or via email at <u>ajuarez@marathonpetroleum.com</u>.

Sincerely,

Alexandra M. Juary G&P Engineer I

cc: MarkWest file

Proof of Delivery

Dear Customer,

This notice serves as proof of delivery for the shipment listed below.

Tracking Number

1Z2E23250395329229

Weight

1.00 LBS

Service

UPS Ground

Shipped / Billed On 06/28/2022

Delivered On

06/29/2022 10:52 A.M.

Delivered To WASHINGTON, PA, US

Received By

JANSETTE

Thank you for giving us this opportunity to serve you. Details are only available for shipments delivered within the last 120 days. Please print for your records if you require this information after 120 days.

Sincerely,

UPS

Tracking results provided by UPS: 06/29/2022 10:55 A.M. EST

Process Flow Diagram



Detailed Emission Estimates

Summary of Potential Emissions

Criteria Pollutant Potential Emissions

D /E 114	C ID	Potential Emissions (lb/hr)								
Process/Facility	Source ID	NOx	СО	VOC	SO ₂	PM ¹	HAPs			
Cryo Plant 1 Regen Heater (H-1711)	031	0.47	0.47	0.22	0.01	0.09	0.02			
Cryo Plant 2 Regen Heater (H-2711)	032	0.78	0.78	0.37	0.01	0.15	0.04			
De-Ethanizer HMO Heater 1 (H-1767)	033	1.93	1.93	0.91	0.03	0.36	0.09			
De-Ethanizer HMO Heater 2 (H-1768)	034	1.93	1.93	0.91	0.03	0.36	0.09			
Stabilization HMO Heater (H-1769)	036	0.48	0.48	0.23	0.01	0.09	0.02			
De-Ethanizer Regen Heater (H-1775)	035	0.26	0.26	0.13	0.00	0.05	0.01			
Process Flare	C601	1.23	5.61	3.07	0.01	0.11	0.22			
Generac SD015	102	0.26	0.14	0.08	0.10	0.02	0.00			
Generac SD150	102	1.31	0.55	0.41	0.10	0.04	0.01			
Fugitives Emissions	701									
Pigging*	801									
Rod Packing	601			0.17			0.00			
Drain Tank Loadout*										
Methanol Tanks				0.08			0.08			
Measurement Devices				0.24			0.02			
Future Site-Wide Emissions (lb/hr)		8.66	12.16	6.84	0.30	1.26	0.60			

 1 PM = PM₁₀ = PM_{2.5}

	a			Potential Emi	ssions (tpy)		
Process/Facility	Source ID	NOx	СО	VOC	SO ₂	PM	HAPs
Cryo Plant 1 Regen Heater (H-1711)	031	2.07	2.07	0.98	0.03	0.39	0.10
Cryo Plant 2 Regen Heater (H-2711)	032	3.44	3.44	1.63	0.05	0.64	0.16
De-Ethanizer HMO Heater 1 (H-1767)	033	8.44	8.44	4.01	0.12	1.57	0.39
De-Ethanizer HMO Heater 2 (H-1768)	034	8.44	8.44	4.01	0.12	1.57	0.39
Stabilization HMO Heater (H-1769)	036	2.10	2.10	1.00	0.03	0.39	0.10
De-Ethanizer Regen Heater (H-1775)	035	1.16	1.16	0.55	0.02	0.22	0.05
Process Flare	C601	5.39	24.56	13.46	0.04	0.50	0.98
Generac SD015	102	0.07	0.04	0.02	0.03	0.01	0.00
Generac SD150	102	0.33	0.14	0.10	0.03	0.01	0.00
Fugitives Emissions	701			10.72			0.50
Pigging*	801						
Rod Packing	601			0.75			0.01
Drain Tank Loadout*							
Methanol Tanks				0.35			0.35
Measurement Devices				1.03			0.08
Future Site-Wide Emissions (tpy)		31.42	50.38	38.62	0.47	5.29	3.10

 1 PM = PM₁₀ = PM_{2.5}

 \ast Emissions are controlled by the flare and thus, are accounted for in the process flare emissions.

Hazardous Air Pollutant Potential Emissions										
Drogogy/Equility	Saumaa ID				HAPs - Po	otential Emissions	(lb/hr)			
Process/Facility	Source ID	Acetaldehyde	Acrolein	Benzene	Ethylbenzene	Formaldehyde	Methanol	n-Hexane	Toluene	Xylenes
Cryo Plant 1 Regen Heater (H-1711)	031			2.44E-05		8.70E-04		0.02	3.95E-05	
Cryo Plant 2 Regen Heater (H-2711)	032			4.04E-05		1.44E-03		0.03	6.54E-05	
De-Ethanizer HMO Heater 1 (H-1767)	033			9.91E-05		3.54E-03		0.08	1.60E-04	
De-Ethanizer HMO Heater 2 (H-1768)	034			9.91E-05		3.54E-03		0.08	1.60E-04	
Stabilization HMO Heater (H-1769)	036			2.47E-05		8.82E-04		0.02	4.00E-05	
De-Ethanizer Regen Heater (H-1775)	035			1.36E-05		4.85E-04		0.01	2.20E-05	
Process Flare	C601									
Generac SD015	102	2.89E-04	3.48E-05	3.51E-04		4.44E-04			1.54E-04	1.07E-04
Generac SD150	102	1.42E-03	1.72E-04	1.73E-03		2.19E-03			7.59E-04	5.29E-04
Fugitives Emissions	701									
Pigging*	801									
Rod Packing	601							0.00		
Drain Tank Loadout*										
Methanol Tanks							8.04E-02			
Measurement Devices								0.02		
Future Site-Wide Emissions (lb/hr)		0.00	0.00	0.00	0.00	0.01	0.08	0.28	0.00	0.00

Drogoss/Epcility	Source ID		HAPs - Potential Emissions (tpy)								
Frocess/Facility	Source ID	Acetaldehyde	Acrolein	Benzene	Ethylbenzene	Formaldehyde	Methanol	n-Hexane	Toluene	Xylenes	
Cryo Plant 1 Regen Heater (H-1711)	031			1.07E-04		3.81E-03		0.09	1.73E-04		
Cryo Plant 2 Regen Heater (H-2711)	032			1.77E-04		6.32E-03		0.15	2.87E-04		
De-Ethanizer HMO Heater 1 (H-1767)	033			4.34E-04		1.55E-02		0.37	7.03E-04		
De-Ethanizer HMO Heater 2 (H-1768)	034			4.34E-04		1.55E-02		0.37	7.03E-04		
Stabilization HMO Heater (H-1769)	036			1.08E-04		3.86E-03		0.09	1.75E-04		
De-Ethanizer Regen Heater (H-1775)	035			5.95E-05		2.13E-03		0.05	9.64E-05		
Process Flare	C601										
Generac SD015	102	7.22E-05	8.70E-06	8.78E-05		1.11E-04			3.85E-05	2.68E-05	
Generac SD150	102	3.56E-04	4.29E-05	4.33E-04		5.47E-04			1.90E-04	1.32E-04	
Fugitives Emissions	701										
Pigging*	801										
Rod Packing	601							0.01			
Drain Tank Loadout*											
Methanol Tanks							3.52E-01				
Measurement Devices								0.08			
Future Site-Wide Emissions (tpy)		0.00	0.00	0.00	0.00	0.05	0.35	1.22	0.00	0.00	

* Emissions are controlled by the flare and thus, are accounted for in the process flare emissions.

Greenhouse Gas Potential Emissions

D /F 114	c D	GHG
Process/Facility	Source ID	CO ₂₍ e) (tpy)
Cryo Plant 1 Regen Heater (H-1711)	031	6857
Cryo Plant 2 Regen Heater (H-2711)	032	11369
De-Ethanizer HMO Heater 1 (H-1767)	033	27893
De-Ethanizer HMO Heater 2 (H-1768)	034	27893
Stabilization HMO Heater (H-1769)	036	6946
De-Ethanizer Regen Heater (H-1775)	035	3824
Process Flare	C601	10622
Generac SD015	102	15
Generac SD150	102	76
Fugitives Emissions	701	306
Pigging*	801	
Rod Packing	601	45
Methanol Tanks		
Measurement Devices		82
Future Site-Wide Emissions (tpy)		95,927.12

* Emissions are controlled by the flare and thus, are accounted for in the process flare emissions.

Potential Emissions Increases from Project

Criteria Pollutant Potential Emissions Increase

Process/Facility	Source ID		Potential Emissions (lb/hr)								
Flocess/Facility	Source ID	NOx	со	VOC	SO2	PM1	HAPs				
Cryo Plant 2 Regen Heater (H-2711)	032	0.78	0.78	0.37	0.01	0.15	0.04				
Process Flare	C601	0.00	0.00	0.00	0.00	0.00	0.00				
Fugitives Emissions	701										
Pigging (De Minimis)*	801										
Rod Packing (De Minimis)	601			0.00			0.00				
Drain Tank Loadout (De Minimis)*											
Methanol Tanks (De Minimis)				0.04			0.04				
Measurement Devices (Exempt)				0.06			0.00				
Future Site-Wide Emissions (lb/hr)		0.78	0.78	0.47	0.01	0.15	0.08				
1 PM = PM10 = PM2.5											

Brooss/Fasility	Source ID		Potential Emissions (tpy)								
r rocess/r aciiity	Source ID	NOx	СО	VOC	SO2	PM1	HAPs				
Cryo Plant 2 Regen Heater (H-2711)	032	3.44	3.44	1.63	0.05	0.64	0.16				
Process Flare	C601	0.00	0.00	0.00	0.00	0.00	0.00				
Fugitives Emissions	701			3.95			0.19				
Pigging (De Minimis)*	801										
Rod Packing (De Minimis)	601			0.001			0.00				
Drain Tank Loadout (De Minimis)*											
Methanol Tanks (De Minimis)				0.18			0.18				
Measurement Devices (Exempt)				0.25			0.02				
Future Site-Wide Emissions (tpy)		3.44	3.44	6.02	0.05	0.64	0.54				
1 PM = PM10 = PM2.5											

-

* Emissions are controlled by the flare and thus, are accounted for in the process flare emissions.

Hazardous Air Pollutant Potential Emissions

Process/Facility	Source ID	HAPs - Potential Emissions (lb/hr)								
1 Toccss/Facinity	Source ID	Acetaldehyde	Acrolein	Benzene	Ethylbenzene	Formaldehyde	Methanol	n-Hexane	Toluene	Xylenes
Cryo Plant 2 Regen Heater (H-2711)	032			4.04E-05		1.44E-03		3.46E-02	6.54E-05	
Process Flare	C601									
Fugitives Emissions	701									
Pigging (De Minimis)*	801									
Rod Packing (De Minimis)	601							1.59E-07		
Drain Tank Loadout (De Minimis)*										
Methanol Tanks (De Minimis)							4.02E-02			
Measurement Devices (Exempt)								4.21E-03		
Future Site-Wide Emissions (lb/hr)		0.00E+00	0.00E+00	4.04E-05	0.00E+00	1.44E-03	4.02E-02	3.88E-02	6.54E-05	0.00E+00

Process/Facility	Source ID	HAPs - Potential Emissions (tpy)								
r tocess/F actinty	Source ID	Acetaldehyde	Acrolein	Benzene	Ethylbenzene	Formaldehyde	Methanol	n-Hexane	Toluene	Xylenes
Cryo Plant 2 Regen Heater (H-2711)	032			1.77E-04		6.32E-03		1.52E-01	2.87E-04	
Process Flare	C601									
Fugitives Emissions	701									
Pigging (De Minimis)*	801									
Rod Packing (De Minimis)	601							6.95E-07		
Drain Tank Loadout (De Minimis)*										
Methanol Tanks (De Minimis)							1.76E-01			
Measurement Devices (Exempt)								1.84E-02		
Future Site-Wide Emissions (tpy)		0.00E+00	0.00E+00	1.77E-04	0.00E+00	6.32E-03	1.76E-01	1.70E-01	2.87E-04	0.00E+00

* Emissions are controlled by the flare and thus, are accounted for in the process flare emissions.

Greenhouse Gas Potential Emissions

Process/Facility	Source ID	GHG
r rocess/r activity	Source ID	CO2(e) (tpy)
Cryo Plant 2 Regen Heater (H-2711)	032	1.14E+04
Process Flare	C601	0.00E+00
Fugitives Emissions	701	1.01E+02
Pigging (De Minimis)*	801	
Rod Packing (De Minimis)	601	1.50E+01
Drain Tank Loadout (De Minimis)*		
Methanol Tanks (De Minimis)		2.02E+01
Future Site-Wide Emissions (tpy)		11,504.66

* Emissions are controlled by the flare and thus, are accounted for in the process flare emissions.

Cryo Plant II Regen Heaters H-2711

Source Designation:	
Manufacturer:	Tulsa Heaters
Year Installed	Planned 2023
Fuel Used:	Natural Gas
Higher Heating Value (HHV) (Btu/scf):	1,153
Max Design Heat Release (mmbtu/hr)	17.84
Heat Release (HHV) (mmbtu/hr)	19.62
Fuel Consumption (mmscf/hr):	0.0170
Potential Annual Hours of Operation (hr/yr):	8,760

Criteria and Manufacturer Specific Pollutant Emission Rates

	Emission Factor	Potential Emissions			
Pollutant	(lb/mmbtu) (lb/MMscf) ^{a,b}	(lb/hr) ^c	(tons/yr) ^d		
NOx	0.04	0.785	3.438		
СО	0.04	0.785	3.438		
VOC	0.019	0.373	1.633		
SO ₂	0.68	0.0115	0.0506		
PM Total	8.59	0.1462	0.6404		
PM Condensable	6.44	0.110	0.480		
PM ₁₀ (Filterable)	2.15	0.037	0.160		
PM _{2.5} (Filterable)	2.15	0.037	0.160		
CO ₂	59.9 kg/mmbtu	2,593	11,357		
CH_4	0.001 kg/mmbtu	0.04890	0.214		
N ₂ O	0.0001 kg/mmbtu	0.00489	0.021		

Hazardous Air Pollutant (HAP) Potential Emissions

	Emission Factor	Potential Emissions		
Pollutant	(lb/MMscf) ^a	(lb/hr) ^c	(tons/yr) ^d	
HAPs				
3-Methylchloranthrene	2.03E-06	3 46E-08	1 52E-07	
7.12-Dimethylbenz(a)anthracene	1.81E-05	3.08E-07	1.35E-06	
Acenaphthene	2.03E-06	3.46E-08	1.52E-07	
Acenaphthylene	2.03E-06	3.46E-08	1.52E-07	
Anthracene	2.71E-06	4.62E-08	2.02E-07	
Benz(a)anthracene	2.03E-06	3.46E-08	1.52E-07	
Benzene	2 37E-03	4.04E-05	1 77E-04	
Benzo(a)pyrene	1.36E-06	2.31E-08	1.01E-07	
Benzo(b)fluoranthene	2.03E-06	3.46E-08	1 52E-07	
Benzo(g,h,i)pervlene	1 36E-06	2 31E-08	1.01E-07	
Benzo(k)fluoranthene	2.03E-06	3.46E-08	1 52E-07	
Chrysene	2.03E-06	3.46E-08	1.52E-07	
Dibenzo(a, h) anthracene	1 36E-06	2 31E-08	1.01E-07	
Dichlorobenzene	1.36E-03	2.31E-05	1.01E-04	
Fluoranthene	3.39E-06	5.77E-08	2.53E-07	
Fluorene	3 17E-06	5 39E-08	2 36E-07	
Formaldehyde	8.48E-02	1.44E-03	6.32E-03	
Hexane	2.03E+00	3.46E-02	1.52E-01	
Indo(1.2.3-cd)pyrene	2.03E-06	3.46E-08	1.52E-07	
Phenanthrene	1.92E-05	3.27E-07	1.43E-06	
Pvrene	5.65E-06	9.62E-08	4.21E-07	
Toluene	3.84E-03	6.54E-05	2.87E-04	
Arsenic	2.26E-04	3.85E-06	1.69E-05	
Bervllium	1.36E-05	2.31E-07	1.01E-06	
Cadmium	1.24E-03	2.12E-05	9.27E-05	
Chromium	1.58E-03	2.69E-05	1.18E-04	
Cobalt	9.50E-05	1.62E-06	7.08E-06	
Lead	5.65E-04	9.62E-06	4.21E-05	
Manganese	4.30E-04	7.31E-06	3.20E-05	
Mercury	2.94E-04	5.00E-06	2.19E-05	
Nickel	2.37E-03	4.04E-05	1.77E-04	
Selenium	2.71E-05	4.62E-07	2.02E-06	
	•			
Polycyclic Organic Matter:				
Methylnaphthalene (2-)	2.71E-05	4.62E-07	2.02E-06	
Naphthalene	6.90E-04	1.17E-05	5.14E-05	
Total HAP	2.135	0.036	0.159	

^a Emission factors from manufacturers guarantees on VOC, NOx, and CO in lb/mmbtu. The remainder from AP-42 Section 1.4 "Natural Gas Combustion" Tables 1.4-1, 1.4-2, & 1.4-3 (07/98) for all criteria and HAP pollutants, corrected to site-specific gas heat content.

^b Emission factors for GHG pollutants from 40 CFR Part 98, Subpart C and corrected to site-specific gas heat content.

^c Emission Rate (lb/hr) = Rated Capacity (MMscf/hr) × Emission Factor (lb/MMscf).

^d Annual Emissions $(tons/yr)_{Potential} = (lb/hr)_{Emissions} \times (Maximum Allowable Operating Hours, 8760 hr/yr) \times (1 ton/2000 lb).$

	Owner Ref.: H-711 THM Ref.: MJ17-300								
			ONDI						Ftnt
1		C	OWBUS	STION DESIGN	CONDITIO	NS			& P~
2	Overall Performance:								Rev
4	Operating Case			Design	Norm(F	Rei)	Norm(Rec)	Turndown	
5	Service			Regen Gas He	ater Regen	Gas Heater	Regen Gas Heate	Regen Gas Heate	r
6	Excess Air		mol%	15.0%	15	5.0%	15.0%	15.0%	
7	Calculated Heat Release	e (LHV) MM	BTU/ hr	16.21	1	4.58	13.93	9.26	
8	Guaranteed Efficiency		HR%	84.7%	84	4.7%	84.7%	84.7%	
9	Calculated Efficiency		HR%	87.7%		3.7%	89.1%	92.1%	
10	Radiation Loss		HR%	2.00%		00%	2.00%	2.00%	
11	Flow Rate, Compustion C	Gen./ Imp.	LD/ Nr ∘⊏	1 4 27 / 46	1 1 270	/ 125	1 350 / 409	9,020	
12	Flue Gas Mass Velocity	I (NO)	/ sec ft2	0.378	<u>1 1,379</u> 0	340	0.325	0.216	
14			000112	0.010			0.020	0.210	
15	Fuel(s) Data: G	as 1 Gas 2		Burne	er Design:				
16	M	ol.Wt. Mol.Wt.		OEI	N	- Zeeco USA	A, LLC		
17	LHV BTU/ scf	910 1,037		Тур	e	- Enhanced	IFGR		
18	LHV BTU/ Lb	21,397 20,449		Qua	ntities	- 1		ULTRA Low NOx	
19	P@Burner psig_	<u>150 150 </u>		Mod	lel No	- GLSF-12		Cylindrical	
20	I @ Burner °F	100 100		Win	abox	- yes EndWall C	enter	Horizontally Fired	
21	www	10.14 19.24		LOC	auuri Desian		01101	HUNZUINAILY FILEU	
22	m @ 222 °F cp =			FIUL	e / Model	Self-Inspi	rating /	by O F M	
24	Atomizing Media			lani	tion	- Electric	req	uires elec.ign.system	
25	Atom. Media P & T			Hea	t Release -	- > 90000	BTU/ hr or	n Gas 1	
26	_								
27	Components:			Burne	er Performa	nce:			
28	N wt%			Min	mum Heat I	Release	MMBTU/ hr	3.57	
29	S wt% _	<u> </u>		Des	ign Heat Re	elease	MMBTU/ hr	16.21	1
30	Ash wt% _			Max	imum Heat	Release	MMBTU/ hr	17.84	
31	NI ppm _			Bur		/n Zalagag	Max:Min	5.00	
3∠ 33	Va ppm			Voit		telease	bTU/ III II inH2O	0,307	
34	Fe ppm			Pre	ssure @ Ait	rner	inH2O	4 35	
35	10 ppm _			Cor	nbustion Air	T @ Burner	· °F	60	
36	H2 mol%	0.0% 0.0%		Flue	Gas T @ E	Burner	°F	1,230	
37	O2 mol%	0.0% 0.0%			U				
38	N2 + Ar mol%	0.2% 1.5%		Guar	anteed Emi	ssions:			
39	CO mol%	0.0% 0.0%		Bas	is of Guarar	ntee		3.0% O2, dry (LHV)	1
40	CO2 mol%	0.0% 0.5%		NO:	K Emissions		Lb/MMBTU	0.040 30 ppm	
41	CH4 mol% _	99.3% 80.2%		SO					
42	C2H6 mol% _				Emissions			0.040 49 ppm	
43	C2H4 1101% _	$\frac{0.0\%}{0.0\%}$				> :		0.019 15 ppm	J
45	C3H6 mol%	0.0% $2.4%$		SPI	A10 Emissions	, ons	Lb/MMBTU	0.013 15 ppm	
46	C4H10 mol%	0.0% 0.2%		Nois	se Emission	S	dBA @ 3ft	85	
47	C4H8 mol%	0.0% 0.0%					0		
48	C5H12 mol%	0.0% 0.0%		Net F	lame Clear	ances:			
49	C5H10 mol%	0.0% 0.0%		Est.	Flame Size	approx. 1	4 ft L x 3 ft Diame	ter	
50	C6+ mol%	0.0% 0.0%		Hor	Clearance	1.5 ft NE	Tube Clearance		
51	H2S ppmv	0.0% 0.0%		Vert	Clearance	1.5 ft NE	I Tube Clearance		
52				Axia	Clearance	10.08 ft NE	LI Retractory Cleara	ance (to Arch hot face))
53	H2O mol%			Nom	inal Flame (learances			
55	spare mol%	0.0% 0.0%		from	burner Cl	\	/ertical	Horizontal	
56		0.070		to T	ube CL. AP	 I ft	8.94	5.96	
57				to T	ube CL. cal	c. ft	4.50	4.50	
58	Blower/Fan Peformance:			to F	efrac., calc.	ft	n/a	24.08	
59	Volumetric Flow	acfm <u>3,</u> 80	0			•			
60	Rated Power	HP 7.5							1
61	Fan Speed	RPM 1,80	0						1
62	Sound Pressure) 	Groups CPD					
03 64	Area Classification		אוט, וו. וו	, Groups C&D					
04									
ll 🛛	AMERICAN EI	NGINEERING SYS	TEM of l	UNITS		FIRE	ED HEATER DAT	A SHEET	
	TULSA H	EATERS MIDSTRI	EAM LLO	С	MJ17-3	300-HTRds-	Rev. 1	Page 2	2 of 6

Flare

Source Designation:	
Manufacturer:	John Zink
Operating Hours: (hr/yr)	8,760
Pilot + Purge Gas Heat Input (MMBtu/hr)	3.205
Pilot + Purge Gas Annual Fuel Use (mmscf/yr)	26.518
Pilot Fuel Consumption (mmscf/hr):	2.00E-04
Purge Fuel Consumption (mmscf/hr):	2.83E-03
Fuel HHV (Btu/scf)	1,059

Combustion of Hydrocarbons

Source Designation:	
Annual Gas Flow (mmscf/yr)	100.00
Heating value (btu/scf)	1,303.99
Maximum Heat Release of Flare (mmbtu/yr)	130,399

Total Emissions

Pollutant	Emission Factor (lb/MMBtu)	lb/hr	tpy
VOC		3.07	13.46
HAP		0.22	0.98
NO _X	0.068	1.23	5.39
СО	0.31	5.61	24.56
SO_2	0.0005	0.01	0.04
PM Total	0.0063	0.11	0.50
PM Condensable	0.0047	0.09	0.37
PM ₁₀ (Filterable)	0.0016	0.03	0.12
PM _{2.5} (Filterable)	0.0016	0.03	0.12
CO ₂	117.05	2119.50	9283.43
CH ₄	0.002	12.18	53.33
N ₂ O	0.0002	0.00	0.02

^a The NOx and CO emission factors are from AP-42 Section 13.5 "Industrial Flares" Table 13.5-1.

 $^{\rm b}$ Emission factors for GHG pollutants from 40 CFR Part 98, Subpart C. Tables C-1 and C-2.

^c The remaining factors are from AP-42 Section 1.4 "Natural Gas Combustion" Tables 1.4-1 and 1.4-2.

^d VOC and HAP emissions are based on mass balance.

^e The flare calculations assume the composition to the flare is inlet gas. Additionally, the flare volume is conservative as the actual flow to the flare during the 2019 reporting period was approximately 26.5

Condensate Truck Loadout Emissions

Source	Volume Loaded (gal/yr)	Saturation Factor ¹	Vapor Pressure ² (psia)	Vapor Molecular Weight ² (lb/lb-mol)	Liquid Temp ³ (ºF)	Liquid Temp (°R)	Loading Loss ⁴ (lb VOC/1000 gal)	Loadir (lb/yr)	ng Loss (tpy)
Harmon Creek Closed Drain Tank	220,000	0.6	8.1621	60	58.5	518.2	7.1	1,554.44	0.78

¹ From AP-42 Table 5.2-1, for tank trucks in submerged loading: dedicated normal service

² From AP42 Table 7.1-2, Gasoline (RVP 15), 60 deg

³ Daily average liquid surface temperature (TANKS 4.09d)

⁴ Loading Loss (lb VOC/1000 gal) = (12.46*S*P*M)/T [AP42 Section 5.2 (1/95)]

⁵ Loading losses are controlled by the flare. Thus, emissions associated with the Condensate Truck Loadout Emissions are captured under the Flare Emission estimates.

Potential VOC Potential HAP Potential CH4 Potential CO2 Stream Type AP-42 Leak Weight Percent^e Total (Gas Vapor. Number of Reduction Final Leak Factor Emissions Emissions Emissions Emissions From Component Type Gas Type Emission Factors Light Liquid, LeakDAS Components lb/hr/component Emissions Factors kg/hr/component^t VOC HAP CH4 **CO2** (lb/hr) (lb/hr) lb/hr) (lb/hr) (tpy) (tpy) (tpy) (tpy) Heavy Liquid) (tpy) GV INLET 8.80E-03 80% 3.88E-03 23.6% 75.1% 0.2% 0.190 0.04 0.14 0.00 0.00 Compressor 11 1.7% 0.01 0.00 0.00 0.03 GV RESIDUE 12 19 8.80E-03 0% 1.94E-02 0.1% 0.0% 87.5% 0.3% 1.633 0.00 0.00 0.00 0.00 0.33 1.43 0.00 0.01 Compressor GV ETHAN 8.80E-03 0% 1.94E-02 0.5% 0.1% 0.0% 0.0% 0.408 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 Compressor CO2 8.80E-03 0% 0.00 0.27 GV 1.94E-02 0.5% 0.1% 0.0% 100.0% 0.272 0.00 0.00 0.00 0.00 0.00 0.06 Compressor GV PROPANE 11 18 8.80E-03 80% 0.0% 0.07 0.30 0.00 0.00 0.00 0.00 0.00 0.00 Compressor 3.88E-03 100.0% 0.0% 0.0% 0.299 INLET 7.50E-03 80% 3.31E-03 23.6% 1.7% 75.1% 0.2% 0.093 0.01 0.02 0.00 0.00 0.02 0.07 0.00 0.00 Compressor INLET GAS 2.00E-04 75% 0.00 0.00 0.00 0.01 0.00 Connector GV 19 30 1.10E-04 23.6% 1.7% 75.1% 0.2% 0.015 0.00 0.00 0.00 GV C3+ 424 678 2.00E-04 75% 0.07 0.33 0.00 0.00 0.00 0.00 Connector 1.10E-04 100.0% 0.0% 0.0% 0.0% 0.328 0.00 0.00 GV **REFRIG C3** 42 67 2.00E-04 75% 100.0% 0.0% 0.0% 0.032 0.01 0.03 0.00 0.00 0.00 0.00 1.10E-04 0.0% 0.00 0.00 Connector GV **REGEN De-Eth** 10 16 2.00E-04 Connector 75% 1.10E-04 0.5% 0.1% 0.0% 0.0% 0.008 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 GV FLARE GAS 1254 2006 2.00E-04 75% 23.6% 0.2% 0.969 0.05 0.23 0.00 0.02 0.17 0.73 0.00 Connector 1.10E-04 1.7% 75.1% 0.00 GV C3+ 2.00E-04 75% 1.10E-04 100.0% 0.0% 0.0% 0.0% 0.001 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 Connector GV INLET 69 110 2.00E-04 75% 1.10E-04 23.6% 1.7% 0.2% 0.053 0.00 0.01 0.00 0.00 0.01 0.04 0.00 0.00 Connector 75.1% GV REGEN GAS De-Eth 13 21 2.00E-04 75% 1.10E-04 0.5% 0.1% 0.0% 0.0% 0.010 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 Connector 2.00E-04 0.00 Connector GV C2+ 112 179 75% 1.10E-04 51.4% 5.3% 0.1% 0.1% 0.087 0.01 0.04 0.00 0.00 0.00 0.00 0.00 GV INLET 252 403 2.00E-04 75% 0.00 Connector 1.10E-04 23.6% 1.7% 75.1% 0.2% 0.195 0.01 0.05 0.00 0.00 0.03 0.15 0.00 GV **REGEN De-Eth** 2.00E-04 75% 1.10E-04 0.5% 0.1% 0.0% 0.0% 0.001 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 Connector GV C3+ 2.00E-04 75% 1.10E-04 100.0% 0.0% 0.0% 0.002 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 Connector 0.0% FLARE GAS 2.10E-04 75% 0.00 0.00 0.00 11 1.16E-04 23.6% 1.7% 0.2% 0.001 0.00 0.00 0.00 0.00 0.00 Connector 75.1% METHANOL LL 102 163 2.10E-04 75% 1.16E-04 100.0% 100.0% 0.0% 0.0% 0.083 0.02 0.08 0.02 0.08 0.00 0.00 0.00 0.00 Connector REGEN GAS De-Eth 108 173 2.10E-04 75% 0.088 0.00 0.00 0.00 0.00 0.00 0.00 0.00 Connector ш 1.16E-04 0.5% 0.1% 0.0% 0.0% 0.00 11 ETHAN 47 75 2.10E-04 75% 1.16E-04 0.5% 0.1% 0.0% 0.0% 0.038 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 Connector ETHAN 32 Connector ш 20 2.10E-04 75% 1.16E-04 0.5% 0.1% 0.0% 0.0% 0.016 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 C3+ 1371 857 2.10E-04 75% 0.00 0.00 Connector LL 1.16E-04 100.0% 0.0% 0.0% 0.0% 0.696 0.16 0.70 0.00 0.00 0.00 0.00 METHANOL 2.10E-04 75% 0.00 0.02 0.02 0.00 0.00 Connector ш 25 40 1.16E-04 100.0% 100.0% 0.0% 0.0% 0.020 0.00 0.00 0.00 INLET GAS 238 2.10E-04 75% 381 Connector LL 1.16E-04 23.6% 1.7% 75.1% 0.2% 0.193 0.01 0.05 0.00 0.00 0.03 0.15 0.00 0.00 Connector LL C3+ 310 496 2.10E-04 75% 1.16E-04 100.0% 0.0% 0.0% 0.0% 0.252 0.06 0.25 0.00 0.00 0.00 0.00 0.00 0.00 INLET GAS 23.6% 100 160 2.10E-04 75% 1.16E-04 1.7% 75.1% 0.2% 0.081 0.00 0.02 0.00 0.00 0.01 0.06 0.00 0.00 Connector ш Pressure Relief GV **REGEN De-Eth** 28 45 8.80E-03 97% 5.82E-04 0.5% 0.1% 0.0% 0.0% 0.114 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 Pressure Relief 747 GV FLARE 467 8.80E-03 97% 5.82E-04 23.6% 1.7% 75.1% 0.2% 1.906 0.10 0.45 0.01 0.03 0.33 1.43 0.00 0.00 FLARE GAS 344 550 8.80E-03 97% 5.82E-04 0.2% 1.404 0.08 0.33 0.02 1.05 0.00 Pressure Relief GV 23.6% 1.7% 75.1% 0.01 0.24 0.00 C3 148 7.50E-03 97% 4.96E-04 0.515 0.12 0.00 0.00 0.00 0.00 Pressure Relief ш 237 100.0% 0.0% 0.0% 0.0% 0.51 0.00 0.00 C2+ 782 1251 7.50E-03 97% 4.96E-04 51.4% 0.00 0.00 Pressure Relief 5.3% 0.1% 0.1% 2.720 0.32 1.40 0.03 0.14 0.00 0.00 Pressure Relief **REGEN GAS De-Eth** 337 539 7.50E-03 97% 4.96E-04 0.5% 0.1% 0.0% 0.0% 1.172 0.00 0.01 0.00 0.00 0.00 0.00 0.00 0.00 11 FLARE 126 7.50E-03 97% 4.96E-04 23.6% 1.7% 0.2% 0.275 0.01 0.06 0.00 0.00 0.05 0.21 0.00 0.00 Pressure Relief 79 75.1% C3+ 7.50E-03 97% 4.96E-04 100.0% 0.0% 0.0% 0.0% 0.014 0.00 0.01 0.00 0.00 0.00 0.00 0.00 Pressure Relief ш 0.00 Pressure Relief 11 REGEN GAS 26 42 7.50E-03 97% 4.96E-04 23.6% 1.7% 75.1% 0.2% 0.090 0.00 0.02 0.00 0.00 0.02 0.07 0.00 0.00 23.6% REGEN GAS 80 128 7.50E-03 97% 0.278 0.02 0.07 0.05 0.21 0.00 Pressure Relief ш 4.96E-04 1.7% 75.1% 0.2% 0.00 0.00 0.00 Pressure Relief C3 403 645 7.50E-03 97% 4.96E-04 100.0% 0.0% 0.0% 0.0% 1.402 0.32 1.40 0.00 0.00 0.00 0.00 0.00 0.00 LL FLARE 2.40E-03 Pump GV 0% 5.29E-03 23.6% 1.7% 75.1% 0.2% 0.186 0.01 0.04 0.00 0.00 0.03 0.14 0.00 0.00 GV FLARE 129 206 2.40E-03 0% 5.29E-03 4.786 0.02 0.82 3.59 0.01 Pump 23.6% 1.7% 75.1% 0.2% 0.26 1.13 0.08 0.00 LL C2+ 10 1.30E-02 85% 51.4% 5.3% 0.181 0.02 0.09 0.00 0.00 0.00 0.00 0.00 Pump 4.30E-03 0.1% 0.1% 0.01

Fugitive Emissions

Fugitive Emissions Potential VOC Potential HAP Potential CH4 Potential CO2 Stream Type AP-42 Leak Weight Percent^e Total (Gas Vapor, Number of Reduction Final Leak Factor Emissions Emissions Emissions Emissions From Component Type Gas Type Emission Factors Light Liquid, LeakDAS Components lb/hr/component Emissions Factors kg/hr/component^t VOC HAP CH4 CO2 (lb/hr) (lb/hr) lb/hr) (lb/hr) (tpy) (tpy) (tpy) (tpy) Heavy Liquid) (tpy) Valve GV REGEN GAS De-Eth 4.50E-03 97% 0.00 63 101 2.98E-04 0.5% 0.1% 0.0% 0.0% 0.131 0.00 0.00 0.00 0.00 0.00 0.00 0.00 4.50E-03 Valve GV C2+ 44 70 97% 2.98E-04 51.4% 5.3% 0.1% 0.1% 0.092 0.01 0.05 0.00 0.00 0.00 0.00 0.00 0.00 Valve GV C3 4.50E-03 97% 2.98E-04 0.0% 0.006 0.00 0.00 0.00 0.00 100.0% 0.0% 0.0% 0.00 0.01 0.00 0.00 Valve GV INLET GAS 44 70 4.50E-03 97% 2.98E-04 23.6% 1.7% 75.1% 0.2% 0.092 0.00 0.02 0.00 0.00 0.02 0.07 0.00 0.00 Valve GV C3+ 113 181 4.50E-03 97% 0.00 0.00 2.98E-04 100.0% 0.0% 0.0% 0.236 0.05 0.24 0.00 0.00 0.00 0.00 0.0% GV C3 489 4.50E-03 97% Valve 782 2.98E-04 100.0% 0.0% 0.0% 0.0% 1.021 0.23 1.02 0.00 0.00 0.00 0.00 0.00 0.00 **REFRIG C3** Valve GV 154 246 4.50E-03 97% 2.98E-04 100.0% 0.0% 0.321 0.07 0.32 0.00 0.00 0.00 0.00 0.00 0.0% 0.0% 0.00 Valve GV INLET 12 19 4.50E-03 97% 2.98E-04 23.6% 1.7% 75.1% 0.2% 0.025 0.00 0.01 0.00 0.00 0.00 0.02 0.00 0.00 Valve GV REFRIG C3 з 4.50E-03 97% 2.98E-04 100.0% 0.0% 0.0% 0.0% 0.004 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 Valve GV C3 140 224 4.50E-03 97% 2.98E-04 100.0% 0.0% 0.0% 0.0% 0.292 0.07 0.29 0.00 0.00 0.00 0.00 0.00 0.00 51.4% 0.00 Valve Π. C2+ 290 464 2.50E-03 97% 1.65E-04 5.3% 0.1% 0.1% 0.336 0.04 0.17 0.00 0.02 0.00 0.00 0.00 Valve LL INLET 935 1496 2.50E-03 97% 1.65E-04 23.6% 1.7% 75.1% 0.2% 1.084 0.06 0.26 0.00 0.02 0.19 0.81 0.00 0.00 2.50E-03 Valve REGEN GAS 97% 0.00 0.00 0.00 0.00 LL 1.65E-04 23.6% 1.7% 75.1% 0.2% 0.002 0.00 0.00 0.00 0.00 Valve LL METHANOL 2.50E-03 97% 1.65E-04 100.0% 100.0% 0.0% 0.0% 0.002 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 Valve INLET 390 624 2.50E-03 97% 1.65E-04 23.6% 0.452 11 1.7% 75.1% 0.2% 0.02 0.11 0.00 0.01 0.08 0.34 0.00 0.00 Valve LL C3+ 2.50E-03 97% 1.65E-04 100.0% 0.0% 0.0% 0.0% 0.002 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 2.50E-03 Valve METHANOL 97% 1.65E-04 100.0% 100.0% 0.0% 0.0% 0.001 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 LL Valve LL **REFRIG C3** 181 290 2.50E-03 97% 1.65E-04 100.0% 0.0% 0.0% 0.0% 0.210 0.05 0.21 0.00 0.00 0.00 0.00 0.00 0.00 Valve LL REFRIG C3 92 147 2.50E-03 97% 1.65E-04 100.0% 0.0% 0.0% 0.0% 0.107 0.02 0.11 0.00 0.00 0.00 0.00 0.00 0.00 2.50E-03 23.6% Valve LL FLARE 19 30 97% 1.65E-04 1.7% 75.1% 0.2% 0.022 0.00 0.01 0.00 0.00 0.00 0.02 0.00 0.00 2.50E-03 Valve LL FLARE 97% 1.65E-04 23.6% 1.7% 75.1% 0.2% 0.003 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 Connector HL нмо 1708 7.50E-06 0% 1.65E-05 100.0% 0.0% 0.0% 0.0% 0.124 0.03 0.12 0.00 0.00 0.00 0.00 0.00 0.00 нмо Valve 569 8.40E-06 0% 0.046 0.01 0.05 0.00 0.00 HL 1.85E-05 100.0% 0.0% 0.0% 0.0% 0.00 0.00 0.00 0.00 Pressure Relief HL нмо 16 3.20E-05 0% 7.06E-05 100.0% 0.0% 0.0% 0.0% 0.005 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 CO2 569 7.50E-06 0% 1.65E-05 0.00 0.01 0.04 Connector HL 0.5% 0.1% 0.0% 100.0% 0.041 0.00 0.00 0.00 0.00 0.00 Valve HL CO2 190 8.40E-06 0% 1.85E-05 0.5% 0.1% 0.0% 100.0% 0.015 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.02 Pressure Relief HL CO2 3.20E-05 0% 7.06E-05 0.5% 0.1% 0.0% 100.0% 0.002 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 Residue Connector GV 1900 2.00E-04 75% 1.10E-04 0.1% 0.0% 87.5% 0.3% 0.918 0.00 0.00 0.00 0.00 0.18 0.80 0.00 0.00 Valve GV Residue 600 4.50E-03 97% 2.98E-04 0.1% 0.0% 87.5% 0.3% 0.783 0.00 0.00 0.00 0.00 0.16 0.69 0.00 0.00 21.343 Total 2.45 10.72 0.11 0.50 2.79 12.23 0.09 0.38

Notes:

^a Component counts are based on a combination of counts from LeakDas and PIDs and estimates based on studies at similar facilities.

^b Table 2-4. Oil & Gas Production Operations Average Emission Factors, Protocol for Equipment Leak Emission Estimates, EPA 453/R-95-017, November 1995. Emission factors based on average measured TOC from component types indicated in gas or light oil service at O&G Production Operations.

^c Table V: Control Efficiencies for LDAR for 28VHP programs, Air Permit Technical Guidance for Chemical Sources Fugitive Guidance, TCEQ (APDG 6422v2, Revised 06/2018). Compressors are monitored quarterly via OGI.

^d Table 5-1. Summary of Equipment Modifications, Protocol for Equipment Leak Emission Estimates, EPA 453/R-95-017, November 1995.

 $^{\rm e}\,$ CO2 and C2 service are estimated at 0.5 VOC wt% to be conservative.

MarkWest Liberty Midstream & Resources, L.L.C. Harmon Creek Gas Plant Rod Packing Emissions

Rod Packing

Total Rod Packing Emissions

Dollutant	Emissions			
Pollulani	lb/hr	tpy		
VOC	0.17	0.75		
Total HAPs	0.00	0.01		
Methane	0.41	1.81		
Carbon Dioxide	0.00	0.01		
n-Hexane	0.00	0.01		
Total HAPs	0.00	0.01		

Residue Compressors Emission Factor^a (scf CH₄/min) 0.018 Mole fraction Methane 0.930 0.019 **Total Emission Factor** (scf/min) MW (lb/lbmole) 17.041 Number of Compressors 7 0.366 **Total Emissions** (lb/hr) ^aBased on 40 CFR Part 98 Subpart W Section 233 Emissions Factors

Dollutant	Mass 9/	Emissions		
Pollulani	IVIdSS %	lb/hr	tpy	
VOC	0.15%	0.00	0.00	
Total HAPs	0.00%	0.00	0.00	
Methane	87.54%	0.32	1.40	
Carbon Dioxide	0.31%	0.00	0.01	
n-Hexane	0.00%	0.00	0.00	
Total HAPs	0.00%	0.00	0.00	

Stabilization Compressors		
Emission Factor ^a	0.018	(scf CH ₄ /min)
Mole fraction Methane	0.440	
Total Emission Factor	0.041	(scf/min)
MW	29.162	(lb/lbmole)
Number of Compressors	2	
Total Emissions	0.378	(lb/hr)
^a Based on 40 CFR Part 98 Subpar	t W Section	233 Emissions Factors

Pollutant	Macc 9/	Emissions		
	IVIdSS 70	lb/hr	tpy	
VOC	44.89%	0.17	0.74	
Total HAPs	0.60%	0.00	0.01	
Methane	24.26%	0.09	0.40	
Carbon Dioxide	0.24%	0.00	0.00	
n-Hexane	0.60%	0.00	0.01	
Total HAPs	0.60%	0.00	0.01	

0.018	(scf CH ₄ /min)
0.025	
0.719	(scf/min)
43.568	(lb/lbmole)
1	
4.960	(lb/hr)
rt W Section	233 Emissions Factors
	0.018 0.025 0.719 43.568 1 4.960 rt W Section

 Pollutant
 Mass %
 Emissions

 VOC
 0.02%
 0.00
 0.00

 Total HAPs
 0.00%
 0.00
 0.00

Total HAPs	0.00%	0.00	0.00
Methane	0.01%	0.00	0.00
Carbon Dioxide	97.82%	0.00	0.00
n-Hexane	0.00%	0.00	0.00
Total HAPs	0.00%	0.00	0.00

Pigging Emissions (Controlled by Flare)

Description		Pressure	High to Low	Control	L/P	Sizo	Max	Pressure (PSIG) ^a	Temp	Vessel	Z Factor ^a	D Fastar ^b	MW of	Maximur	n Volume	Control	led VOC	Control	led HAP
Description	Gas Source Basis	Туре	Jumper	Device	L/K	Events/Yr	Pre-Jump	(deg F)	(acf)	Pre-Jump	K Factor	Gas ^a	Per Event (scf)	Annually (scf/yr)	Wt% ^a	tpy ^c	Wt% ^a	tpy ^c	
Houston Plant HP NGL Launcher	Harmon Creek Plant	HP	N	Flare	Launcher	12	1	1100	85	19.04	0.956	1,545	21.6	1,509.8	1,510	23.6%	0.000	1.72%	0.0000
Mariner West HP Ethane Launcher	Harmon Creek Plant	HP	N	Flare	Launcher	10	1	1100	85	15.95	0.956	1,545	21.6	1,264.8	1,265	23.6%	0.000	1.72%	0.0000
National Fuel Line N HP Residue Launcher	Harmon Creek Plant	HP	N	Flare	Launcher	20	1	1300	85	55.07	0.956	1,545	21.6	5,150.3	5,150	23.6%	0.001	1.72%	0.0001
Rover HP Interconnect Launcher	Harmon Creek Plant	HP	N	Flare	Launcher	24	1	1300	85	108.94	0.758	1,545	21.6	12,852.0	12,852	23.6%	0.002	1.72%	0.0002
Smith CS to Harmon Creek Plant HP Receiver	Harmon Creek Plant	HP	N	Flare	Receiver	20	365	1060	54.2	26.50	0.956	1,545	21.0	2,025.9	739,460	20.2%	0.099	1.67%	0.0082
				Total											760,236		0.102		0.008

* Pigging emissions are controlled by the flare and emission associated with pigging events are accounted for in the flare emissions section.

^a Actual factors for PSIG, Z-factor, MW of gas, VOC wt% of gas and LHV of gas have been calculated but the numbers in the spreadsheet are provided to be very conservative in the event that the composition of the gas field changes over time.

^b R Factor = (psfa*ft3* lbmol/(lb*R))

^c Per the Consent Decree filed in April 2018, the mass of VOC emissions from pigging operations are multiplied by a factor of:

1.2

 CO2 wt%
 0.24%

 CH4 wt%
 75.1%

 CO2 emissions
 0.001
 tpy

 CH4 emissions
 0.32
 tpy

Methanol Emission Estimates

Source Information:	
Contents:	Methanol
Quantity:	2
Tank Orientation/Geometry:	Horizontal Cylinder
Approx. Height (ft):	5.0
Approx. Diameter (ft):	4.2
Volume (gal):	500
Turnovers per year:	0.10
Maximum Fill Level:	90%
Insulation:	None
Tank Color:	Red
Control Percentage:	0
Site-Wide Throughput (gal/yr)	100
Site-Wide Throughput (bbl/day)	0.007

Total Methanol Emissions (Sum of Tank Emissions + Process Emissions below):

	Conservative Losses				
Pollutant	lb/hr	tpy			
Total VOC	0.080	0.352			
Total HAP	0.080	0.352			

Tank Emissions:

	Tank Losses			
Pollutant	lb/hr	tpy		
Total VOC	0.003	0.013		
Total HAP	0.003	0.013		

Methanol tank losses are conservatively based on 50 gallons of use annually and modeled using ProMax 5.0. Please note, MarkWest uses no more than five (5) gallons of methanol per year.

Process Emissions:

	Conservativ	ve Losses
Pollutant	lb/hr	tpy
Total VOC	0.077	0.339
Total HAP	0.077	0.339

Methanol losses from the process conservatively assumes all methanol injected into the system is emitted to the atmosphere, however, only a portion of the injected methanol will be emitted. Additionally, MarkWest uses no more than five (5) gallons of methanol per year, however, emission estimates are based on 10 times that quantity. Sample Calculation:

Methanol emissions (tpy) = Methanol usage (gal/yr) * Density (lb/gal) / 2000 (ton/lbs)

Measurement Devices

Exempt under Section 127.14(a) #7

Source Information:	
Analyzer Vent Rate (scf/hr)	2.12
Spectra Analyzers	8.00
GC Vent Rate (scf/hr)	0.04
GC Streams	17.00
Total Number of Measurement Vents to Atm	25.0
Potential Annual Hours of Operation (hr/yr)	8,760
Potential Volume Emitted (scf/yr)	18,561

Dollutant	Per An	nalyzer	Per GC	Stream	Total		
Follutalit	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	
Carbon Dioxide	0.000	0.001	0.000	0.000	0.00	0.011	
Methane	0.09	0.397	0.00	0.007	0.75	3.285	
VOC	0.03	0.125	0.00	0.002	0.24	1.033	
n-Hexane	2.07E-03	0.009	3.45E-05	0.000	0.02	0.075	
Total HAPs	2.07E-03	0.009	3.45E-05	0.000	0.02	0.075	

Harmon Creek Gas Analysis

				Residue				
				Gas -	Residue	Stabilizer		
Component	MW	Unit	Inlet Gas	Recovery	Gas	Overhead	CO2	C2+
Nitrogen	28.0135	mole %	0.44	0.51	0.48	0.10	0.00	0.00
CO2	44.01	mole %	0.12	0.20	0.12	0.16	96.84	0.06
H2S	34.1	mole %	0.00	0.00	0.00	0.00	0.00	0.00
Methane	16.042	mole %	75.08	97.41	92.99	44.04	0.03	0.10
Ethane	30.069	mole %	15.76	1.84	6.35	29.62	3.12	59.23
Propane	44.096	mole %	5.12	0.04	0.06	17.14	0.02	23.38
i-Butane	58.122	mole %	0.53	0.00	0.00	1.86	0.00	2.95
n-Butane	58.122	mole %	1.40	0.00	0.00	4.96	0.00	7.05
i-Pentane	72.149	mole %	0.32	0.00	0.00	0.79	0.00	1.69
n-Pentane	72.149	mole %	0.45	0.00	0.00	1.06	0.00	2.18
n-Hexane	86.175	mole %	0.43	0.00	0.00	0.20	0.00	3.46
n-Heptane	100.202	mole %	0.32	0.00	0.00	0.05	0.00	0.00
n-Octane	114.229	mole %	0.01	0.00	0.00	0.00	0.00	0.00
n-Nonane	128.255	mole %	0.00	0.00	0.00	0.00	0.00	0.00
n-Decane	142.282	mole %	0.00	0.00	0.00	0.00	0.00	0.00
				Residue				
				Gas -	Residue	Stabilizer		
Component	MW	Unit	Inlet Gas	Recovery	Gas	Overhead	CO2	C2+
Nitrogen	28.0135	wt%	0.5707	0.8738	0.7852	0.0965	0.0000	0.0000
CO2	44.01	wt%	0.2445	0.5278	0.3121	0.2440	97.8220	0.1187

	Component	MW	Unit	Inlet Gas	Recovery	Gas	Overhead	CO2	C2+
23	Nitrogen	28.0135	wt%	0.5707	0.8738	0.7852	0.0965	0.0000	0.0000
24	CO2	44.01	wt%	0.2445	0.5278	0.3121	0.2440	97.8220	0.1187
25	H2S	34.1	wt%	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
26	Methane	16.042	wt%	75.0800	95.1232	87.5426	24.2604	0.0092	0.0736
27	Ethane	30.069	wt%	21.9424	3.3662	11.2128	30.5465	2.1522	48.5233
28	Propane	44.096	wt%	10.4539	0.1031	0.1442	25.9200	0.0166	27.2355
29	i-Butane	58.122	wt%	1.4263	0.0025	0.0011	3.7135	0.0000	3.8104
30	n-Butane	58.122	wt%	3.7677	0.0035	0.0013	9.8881	0.0000	9.4580
31	i-Pentane	72.149	wt%	1.0690	0.0000	0.0002	1.9617	0.0000	2.4280
32	n-Pentane	72.149	wt%	1.5033	0.0000	0.0005	2.6260	0.0000	3.1565
33	n-Hexane	86.175	wt%	1.7158	0.0000	0.0001	0.5960	0.0000	5.3212
34	n-Heptane	100.202	wt%	1.4847	0.0000	0.0000	0.1622	0.0000	0.0000
35	n-Octane	114.229	wt%	0.0529	0.0000	0.0000	0.0192	0.0000	0.0000
36	n-Nonane	128.255	wt%	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
37	n-Decane	142.282	wt%	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
	*Dry Basis		VOC wt %	23.62	0.11	0.15	44.89	0.02	51.41
			LHV =	1178.81	916.57	949.85	1562.36	51.09	
			HHV =	1303.99	1022.94	1058.62	1715.11	61.37	
			Density (Ib	0.0569	0.0433	0.0449	0.0768	0.1148	
			Gas MW=	21.60	16.43	17.04	29.16	43.57	
			HAP wt%=	1.7158	0.0000	0.0001	0.5960	0.0000	5.3212

Notes:

^a The inlet gas composition is based on a sample collected on 6/3/2021 from the Harmon Creek plant feed inlet and a 10% factor is applied for conservatism. An inlet sample analyzed in 2022, see appended, was lower in VOC than the 2021 sample. The residue gas and C2+ gas compositions are the annual average from GC readings.

^b Stabilizer Overhead and CO2 compositions are modeled.



Certificate of Analysis

Vessel / Object:	TBD	Job No:	178-21-00177
Location:	Bulger, PA / MarkWest - Harmon Creek Facility (United States)	Date Sampled:	06/03/21
Job Type:	Sample & Analysis	Date Tested:	06/15/21
Product Grade:	Other Pressurized Product	Version:	1 / 15 Jun 2021 18:45
Client Reference:	MarkWest Liberty Resources / Phillip Jereza		

Sample

178-21-00177-001

Sample ID, Type & Description

Harmon Creek Inlet Gas Line

Method	Test	Result	<u>Units</u>
ASTM D1945	Natural Gas Analysis		
	Hydrogen	0.02	Mol %
	Oxygen	< 0.01	Mol %
	Nitrogen	0.44	Mol %
	Carbon Dioxide	0.12	Mol %
	Methane	75.08	Mol %
	Ethane	15.76	Mol %
	Propane	5.12	Mol %
	Isobutane	0.53	Mol %
	n-Butane	1.40	Mol %
	Isobutylene	0.01	Mol %
	cis-2-Butene	< 0.01	Mol %
	Isopentane	0.32	Mol %
	n-Pentane	0.45	Mol %
	n-Hexane	0.43	Mol %
	n-Heptane	0.28	Mole
	Benzene	0.04	Mol %
	C8+	0.01	Mol %
	Underson O. If de	.04	
ASTM D5504	Hydrogen Suinde	< 0.1	ppmw
ASTM D7423	Oxygenates by FID GC on 400° Cut Back Calculated to Whole Crud	e	
	Acetaldehyde	1.0	ppmw
	Acetone	1.5	ppmw
	Methanol	None Detected	ppmw
	Ethanol	0.9	ppmw
	Total Oxygenates	3.4	ppmw
GPA2286	Full Scan	See Attached	

		Cite	Harmon	
		Sile Somple Nome	Inlet Gas	
Saybolt			13337001	
A CORE LABORATORIES COMPANY		Lap#	6/01/00	
C		Date Sampled	0/21/22	
Customer		Time Sampled		
Markwest		Gas Temp, F		
Harmon Creek		Gas Press, psi		
		Cylinder#		
Pressure base 14.696psi	11	N a she s al	100000001	1
Analysis			1333/991	
Holium	Nol %	GPA 2200	0.02	
Overgon	Mol %		0.02	
Nitrogon	Mol %		0.00	
Carbon Dioxido	Mol %		0.05	
Mothano	Mol %		76.26	
Ethano	Mol %		15.44	
Propage	Mol %		5 10	
Isobutane	Mol %		0.50	
n-Butane	Mol %		1 31	
Isopentane	Mol %		0.25	
n-Pentane	Mol %		0.25	
Hexanes Plus	Mol %		0.51	
Total	Mol %		100.00	
Molecular Weight	#/#-mol		21 19	
Molar Mass Batio			0 7318	
Relative Density			0.7343	
Compressibility Factor			0.9962	
Gross Heating Value (Dry/Ideal)	BTU/CE		1283.3	
Gross Heating Value (Dry/Real)	BTU/CF		1288.2	
Net Heating Value (Dry/Ideal)	BTU/CF		1164.7	
Net Heating Value (Dry/Real)	BTU/CF		1169.1	
@ Pressure base 14.73psi	2.0,0.		110011	
Gross Heating Value (Drv/Ideal)	BTU/CF		1286.3	
Gross Heating Value (Dry/Real)	BTU/CF		1291.2	
Net Heating Value (Drv/Ideal)	BTU/CF		1167.4	
Net Heating Value (Dry/Real)	BTU/CF		1171.8	
2,2-Dimethylbutane	Mol %		0.005	
2-Methyl Pentane	Mol %		0.066	
3-Methyl Pentane	Mol %		0.052	
n-Hexane	Mol %		0.109	
Methylcyclopentane	Mol %		0.015	
Benzene	Mol %		0.004	
Cyclohexane	Mol %		0.015	
2-Methyl Hexane	Mol %		0.027	
3-Methyl Hexane	Mol %		0.023	
Dimethylcyclopentanes	Mol %		0.008	
n-Heptane	Mol %		0.045	
Methylcyclohexane	Mol %		0.030	
Trimethylcyclopentanes	Mol %		0.008	
Toluene	Mol %		0.008	
2-Methylheptane	Mol %		0.026	
3-Methylheptane	Mol %		0.012	
Dimethylcyclohexanes	Mol %		0.007	
n-Octane	Mol %		0.024	
Ethyl Benzene	Mol %		0.000	
Xylenes (Total)	Mol %		0.004	
C9 Naphthenes	Mol %		0.002	
C9 Paraffins	Mol %		0.010	
n-Nonane	Mol %		0.003	
Decanes Plus	Mol %		0.006	
Hexanes Plus Mol Wt	#/#-mol		95.79	
Hexanes Plus Relative Density	60/60		0.6992	
Hexanes Plus Heating Value	BTU/CF (Ideal)		5215.5	
Hexanes Plus Vapor Equivalent	CF/gal		23.09	

Supporting Documentation

Fugitive Components Support Documentation

28	VHP Boilerplate Special Condition Language	MPLX Practices
А	The requirements of paragraphs F and G shall not apply (1) where the Volatile	
	Organic Compound (VOC) has an aggregate partial pressure or vapor pressure of	
	less than 0.044 pounds per square inch, absolute (psia) at 68°F or (2) operating	
	pressure is at least 5 kilopascals (0.725 psi) below ambient pressure. Equipment	
	excluded from this condition shall be identified in a list or by one of the methods	
	described below to be made readily available upon request. The exempted	
	components may be identified by one or more of the following methods:	
	 piping and instrumentation diagram (PID); 	
	 a written or electronic database or electronic file; 	
	 color coding; 	
	 a form of weatherproof identification; or 	
	 designation of exempted process unit boundaries. 	
В	Construction of new and reworked piping, valves, pump systems, and compressor	Construction of new and reworked piping, valves, pump systems, and
	systems shall conform to applicable American National Standards Institute (ANSI),	compressor systems will conform with all applicable codes. The
	American Petroleum Institute (API), American Society of Mechanical Engineers	construction bid language that will be required for Harmon Creek II is
	(ASME), or equivalent codes.	appended.
С	New and reworked underground process pipelines shall contain no buried valves	No new or reworked underground process pipelines are associated
	such that fugitive emission monitoring is rendered impractical. New and	with Harmon Creek. Any new underground drain piping will be
	Te worked buried connectors shall be welded.	Welded.
U	To the extent that good engineering practice will permit, new and reworked	To the extent possible, MPLX ensures that all valves and piping
	valves and piping connections shall be so located to be reasonably accessible for	
	leak checking during plant operation.	
	Difficult-to-monitor and unsafe-to-monitor valves, as defined by Title 30 Texas	There are no difficult-to-monitor or unsafe-to-monitor components at
	Administrative Code Chapter 115 (30 TAC Chapter 115) shall be identified in a list	Harmon Creek Should such components exist at a facility they would
	to be made readily available upon request. The difficult-to-monitor and unsafe-	be identified in a list that is available upon request.
	to-monitor valves may be identified by one or more of the methods described in	
	subparagraph A above. If an unsafe to monitor component is not considered safe	
	to monitor within a calendar year, then it shall be monitored as soon as possible	
	during safe to monitor times. A difficult to monitor component for which	
	quarterly monitoring is specified may instead be monitored annually.	
Ε	New and reworked piping connections shall be welded or flanged. Screwed	MPLX construction practices are consistent with these conditions.
	connections are permissible only on piping smaller than two-inch diameter.	

	Gas or hydraulic testing of the new and reworked piping connections at no less than operating pressure shall be performed prior to returning the components to service or they shall be monitored for leaks using an approved gas analyzer within 15 days of the components being returned to service. Adjustments shall be made as necessary to obtain leak-free performance.	Hydraulic testing of new or reworked piping connections is conducted prior to installation. Any modified piping would undergo field nondestructive examination (NDE). Leak checks are performed prior to putting systems into service.
	Connectors shall be inspected by visual, audible, and/or olfactory means at least weekly by operating personnel walk-through.	Operations conducts daily AVO inspections. LDAR conducts weekly AVO inspections on pumps.
	Each open-ended valve or line shall be equipped with an appropriately sized cap, blind flange, plug, or a second valve to seal the line. Except during sampling, both valves shall be closed.	MPLX's LDAR Program at the facility requires OEVs and OELs to be equipped with an appropriately sized cap, blind flange, plug, or a second valve to seal the line.
	 If the isolation of equipment for hot work or the removal of a component for repair or replacement results in an open ended line or valve, it is exempt from the requirement to install a cap, blind flange, plug, or second valve for 72 hours. If the repair or replacement is not completed within 72 hours, the permit holder must complete either of the following actions within that time period; (1) a cap, blind flange, plug, or second valve must be installed on the line or valve; or (2) the open-ended valve or line shall be monitored once for leaks above background for a plant or unit turnaround lasting up to 45 days with an approved gas analyzer and the results recorded. For all other situations, the open-ended valve or line shall be monitored once within the 72 hour period following the creation of the open ended line and monthly thereafter with an approved gas analyzer and the results recorded. For turnarounds and all other situations, leaks are indicated by readings of 500 ppmv and must be installed on the line or valve 	MPLX's standard is to only allow OELs and/or OEVs to exist on equipment that is not in service and follows the lockout and tagout procedures.
-	Accessible valves shall be monitored by leak checking for fugitive emissions at	Valves are monitored quarterly using Method 21.
	Ieast quarterly using an approved gas analyzer. Sealless/leakless valves (including, but not limited to, welded bonnet bellows and diaphragm valves) and relief valves equipped with a rupture disc upstream or venting to a control device are not required to be monitored. If a relief valve is equipped with rupture disc, a pressure-sensing device shall be installed between the relief valve and rupture disc to monitor disc integrity.	Sealless/leakless valves are not part of the Harmon Creek processes. There will be no relief valves with rupture discs in VOC service. Any relief valves with a rupture disc are equipped with a pressure-sensing device. All valves and relief valves in VOC service are monitored quarterly at Harmon Creek.

	A check of the reading of the pressure-sensing device to verify disc integrity shall be performed at least quarterly and recorded in the unit log or equivalent. Pressure sensing devices that are continuously monitored with alarms are exempt from recordkeeping requirements specified in this paragraph. All leaking discs shall be replaced at the earliest opportunity but no later than the next process shutdown.	There are no relief valves equipped with rupture discs in VOC service at Harmon Creek. However, it is standard that any rupture discs at the facility are equipped with a transmitter or switch which would alarm if the disc failed. Transmitters/switches are considered critical and thus, would be inspected during critical instrumentation rounds.
	The gas analyzer shall conform to requirements listed in Method 21 of 40 CFR part 60, appendix A. The gas analyzer shall be calibrated with methane. In addition, the response factor of the instrument for a specific VOC of interest shall be determined and meet the requirements of Section 8 of Method 21. If a mixture of VOCs is being monitored, the response factor shall be calculated for the average composition of the process fluid. A calculated average is not required when all of the compounds in the mixture have a response factor less than 10 using methane. If a response factor less than 10 cannot be achieved using methane, then the instrument may be calibrated with one of the VOC to be measured or any other VOC so long as the instrument has a response factor of less than 10 for each of the VOC to be measured.	The gas analyzer used for monitoring equipment under this program meets Method 21 requirements.
	Replacements for leaking components shall be re-monitored within 15 days of being placed back into VOC service.	The resurvey requirements described in this section are consistent with MPLX's LDAR Program at the facility.
G	Except as may be provided for in the special conditions of this permit, all pump, compressor, and agitator seals shall be monitored with an approved gas analyzer at least quarterly or be equipped with a shaft sealing system that prevents or detects emissions of VOC from the seal. Seal systems designed and operated to prevent emissions or seals equipped with an automatic seal failure detection and alarm system need not be monitored. These seal systems may include (but are not limited to) dual pump seals with barrier fluid at higher pressure than process pressure, seals degassing to vent control systems kept in good working order, or seals equipped with an automatic seal failure detection and alarm system. Submerged pumps or sealless pumps (including, but not limited to, diaphragm, canned, or magnetic-driven pumps) may be used to satisfy the requirements of this condition and need not be monitored.	All pumps in VOC service are monitored via Method 21 monthly. Compressors in VOC service are monitored at least quarterly via OGI.
Η	Damaged or leaking values or connectors found to be emitting VOC in excess of 500 parts per million by volume (ppmv) or found by visual inspection to be leaking (e.g., dripping process fluids) shall be tagged and replaced or repaired.	values or connectors found to be emitting VOC in excess of 500 ppmv are tagged and replaced or repaired.
		Upon detection of a leak from pump seals or compressor seals, the component is tagged and replaced or repaired.

	Damaged or leaking pump, compressor, and agitator seals found to be emitting	
	VOC in excess of 2,000 ppmv or found by visual inspection to be leaking (e.g.,	
	dripping process fluids) shall be tagged and replaced or repaired.	The first attempt repair requirements described in this section are
	A first attained to remain the lock much be medel within E days and a record of the	consistent with MPLX's LDAR Program at the facility.
	A first attempt to repair the leak must be made within 5 days and a record of the	
1	Δ leaking component shall be repaired as soon as practicable, but no later than 15	The repair requirements described in this section are consistent with
•	days after the leak is found.	MPLX's LDAR Program at the facility.
		···· _··
	If the repair of a component would require a unit shutdown that would create	Emissions from a unit shutdown are evaluated to determine if a DOR
	more emissions than the repair would eliminate, the repair may be delayed until	is appropriate.
	the next scheduled shutdown.	
	All looking components which cannot be repaired until a scheduled shutdown	DOPs are identified with a weatherproof tag and tracked via the
	shall be identified for such renair by tagging within 15 days of the detection of the	LeakDas database
	leak. A listing of all components that gualify for delay of repair shall be	
	maintained on a delay of repair list.	
	The cumulative daily emissions from all components on the delay of repair list	30 TAC 115.782 (c)(1)(B)(i)(II) requires mass emission rates to be
	shall be estimated by multiplying by 24 the mass emission rate for each	calculated using the EPA correlation approach. MPLX uses the
	component calculated in accordance with the instructions in 30 FAC 115.782	LeakDas database to track leaks, which calculates emissions using the
	The calculations of the cumulative daily emissions from all components on the	MPLX has reviewed DOR data and at no point has cumulative daily
	delay of repair list shall be updated within ten days of when the latest leaking	emissions from all components on the DOR list exceeded the
	component is added to the delay of repair list. When the cumulative daily	emissions that would result from the next scheduled shutdown. MPLX
	emission rate of all components on the delay of repair list times the number of	will perform the calculation as required and make the appropriate
	days until the next scheduled unit shutdown is equal to or exceeds the total	notifications to PADEP.
	emissions from a unit shuldown as calculated in accordance with 30 TAC 115.782 (c)(1)(B)(i)(I) the TCEO Begional Manager and any local programs shall be potified	
	and may require early unit shutdown or other appropriate action based on the	
	number and severity of tagged leaks awaiting shutdown. This notification shall be	
	made within 15 days of making this determination.	
J	Records of repairs shall include date of repairs, repair results, justification for	The recordkeeping requirements described in this section are
	delay of repairs, and corrective actions taken for all components.	consistent with MPLX's LDAR Program at the facility.
	Records of instrument monitoring shall indicate dates and times, test methods.	Operations conducts daily AVO inspections via walkthroughs and
	and instrument readings. The instrument monitoring record shall include the time	makes note of such inspections.
	that monitoring took place for no less than 95% of the instrument readings	

	recorded. Records of physical inspections shall be noted in the operator's log or	
	equivalent.	
Κ	Alternative monitoring frequency schedules of 30 TAC "115.352 - 115.359 or	
	National Emission Standards for Organic Hazardous Air Pollutants, 40 CFR Part 63,	
	Subpart H, may be used in lieu of Items F through G of this condition.	
L	Compliance with the requirements of this condition does not assure compliance	
	with requirements of 30 TAC Chapter 115, an applicable New Source Performance	
	Standard (NSPS), or an applicable National Emission Standard for Hazardous Air	
	Pollutants (NESHAPS) and does not constitute approval of alternative standards	
	for these regulations.	

Construction Bid Language

MARKWEST Energy Partners, L.P.

Harmon Creek #1 Project CONSTRUCTION SCOPE of WORK – MECHANICAL, STRUCTURAL & ELECTRICAL

3.0 SPECIFICATIONS

The PROJECT shall be constructed in accordance with all applicable OWNER codes, standards, and specifications as identified in *APPENDIX A*, as well as all applicable Federal, State and local laws, rules, regulations and permit conditions. In addition, the project shall be constructed in accordance with the current edition of the following industry codes, standards, and specifications:

Pressure vessels	ASME VIII Div.1
Air-cooled heat exchangers	API-661 & ASME VIII Div.1
Shell & tube heat exchangers	TEMA class C & ASME VIII Div.1
Plate & frame heat exchangers	ASME VIII Div.1
Fired Heaters	NFPA & API-560
Centrifugal pumps – hydrocarbon	API-610 or ANSI B73
Reciprocating compressors	API-618
Packaged Rotating Eqmt. Lube systems	API-614
Atmospheric Above Ground Tanks	UL-142
Atmospheric FRP Tanks	API-12P
Pipelines – liquid & gas	ASME B31.4 & ASME B31.8 (CFR 49 Parts 195 & 192)
Piping – process & utility	ASME B31.3
Pressure Safety Valves	ASME VIII Div.1
Area classification	API RP-500
Cast-in-place concrete	ACI-318
Masonry Structures	ACI-530
Structural steel	AISC Manual of Steel Construction
Structural steel buildings	AISC 360
Structural steel welding	AWS D1.1
High strength bolting	AISC – Specification for Structural Joints using ASTM A325 or A490 Bolts
International Building Code	IBC
Inspection of Pressure Vessels	NB-23 API-510

Permitting Fees


AIR QUALITY FEES FOR NEW PLAN APPROVAL

Company Information					
Federal Tax ID: 30-0528059			Firm Name: MarkWest Liberty Midstream and Resources, L.L.C.		
Permit # (If any): 63-01011A			Facility Name: Harmon Creek Gas Plant		
Municipality: Smith Township			County: Washington		
Contact Person Name: Allie Juarez			Telephone Number: 412-815-8886		
E-mail: ajuarez@marathonpetroleum.com					
New Plan Approval (The following fees are cumulative.)					
Line #	Check the appropriate boxes below	Type of review requested		Fee 2021 - 2025	Total Fees
1	Base Fee	Subchapter B		\$2,500	\$2,500
2		New Source Review, Subchapter E		\$7,500	
3		NSPS/NESHAP /N A. # of NSPS: B. # of NESHAP/MACT: C. Add lines A and B: D. Maximum applicable standa E. Enter smaller of line C or lin Multiply line E by \$2,500 and e "Total Fees" column.	MACT standard2 ards:3 ne D:2 inter the amount in the	\$5,000	\$5,000
4		Case-by-Ca	Case-by-Case MACT		
5		Prevention of Significant Deterioration (PSD) requirements. Subchapter D		\$32,500	
6		Plantwide Applicability Limit (PAL) for NSR regulated pollutants or PAL for PSD regulated pollutants or both		\$7,500	
7		Risk Assessment Analysis – Inhalation only		\$10,000	
8		Risk Assessment Analysis – Multi-pathway \$25,000		\$25,000	
Add Lines 1 thru 8 of Total Fees column and write it here.					\$7,500